



Turbulence Modelling: LES & DES

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- What is LES?
- Why LES?
- What about the cost?
- What does FLUENT offer
- Best-practice LES with FLUENT
- Closing Remarks

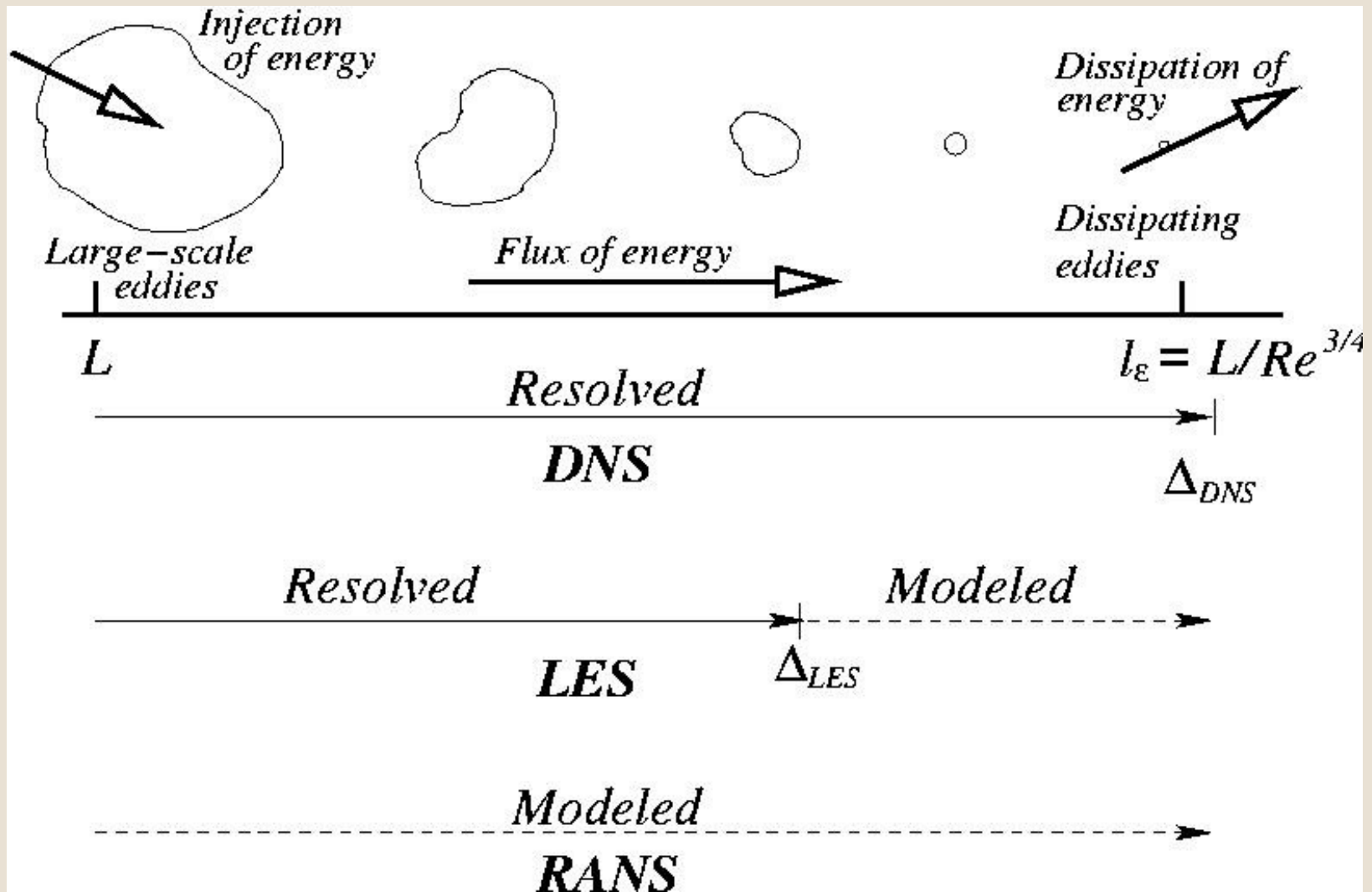
What is LES?

LES: Basic Concepts (1)



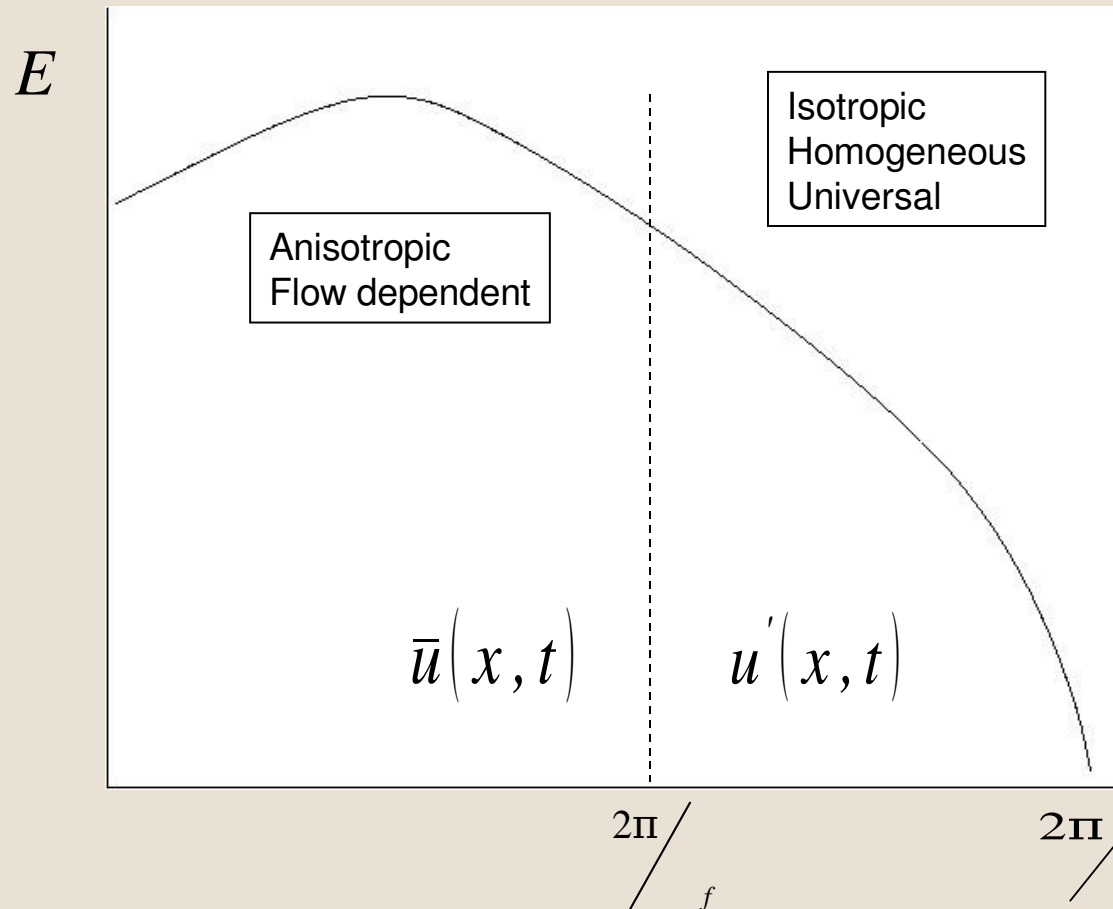
- Turbulent flow consists of eddies (structures) with wide range of length and time scales.
- In LES, large, energy-carrying eddies are directly computed (resolved), and the remaining smaller eddies are modeled.

LES: Basic Concepts (2)



LES: Filtering - Decomposition

$$u(x, t) = \underbrace{\bar{u}(x, t)}_{\text{resolved scale}} + \underbrace{u'(x, t)}_{\text{subgrid scale}}$$



Energy spectrum
against the length scale

LES: Filtering of a Variable

- A random variable, $\phi(x)$, is filtered using a space-filter function, G

$$\bar{\phi}(x) = \int_D \phi(x') G(x, x') dx'$$

- With the top-hat filter (among others)

$$1/V \quad \text{for } \{x' \in \mathcal{V}\}$$

$$G(x, x') = \begin{cases} 1/V & \text{for } \{x' \in \mathcal{V}\} \\ 0 & \text{otherwise} \end{cases}$$

- The filtered variable becomes

$$\bar{\phi}(x) = \frac{1}{V} \int_{\mathcal{V}} \phi(x') dx', \quad \{x \in \mathcal{V}\}$$

LES: Filtered Navier-Stoke Equations

- Filtering the original Navier-Stokes equations gives filtered Navier-Stokes equations that are the governing equations in LES.

N-S equation

$$\frac{\partial u_i}{\partial t} + \frac{\partial u_i u_j}{\partial x_j} = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left(\nu \frac{\partial u_i}{\partial x_j} \right)$$

Filter



Filtered N-S equation

$$\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial \bar{u}_i \bar{u}_j}{\partial x_j} = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} \left(\nu \frac{\partial \bar{u}_i}{\partial x_j} \right) - \frac{\partial \tau_{ij}}{\partial x_j}$$

$$\tau_{ij} \equiv \overline{u_i u_j} - \bar{u}_i \bar{u}_j \longleftarrow \text{Needs modelling}$$

Sub-grid scale (SGS) stress

Why LES? - Rationales

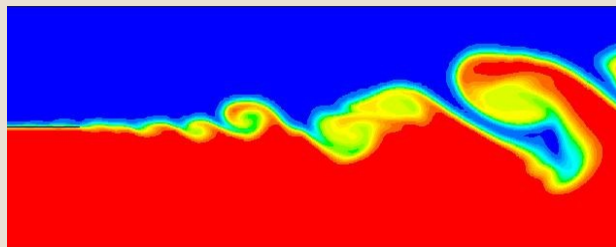


- Large eddies are responsible for the transports of momentum, energy, and other scalars.
- Large eddies are anisotropic, subjected to history effects, and are strongly dependent on boundary conditions, which makes their modelling difficult.
- Small eddies tend to be more isotropic and less flow-dependent (universal), which makes their modelling easier.

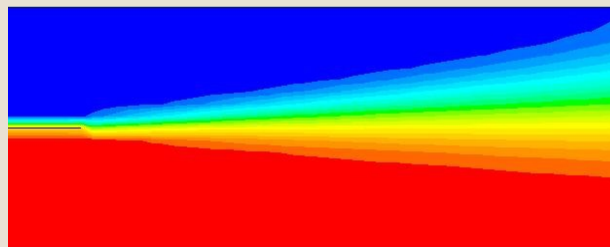
Why LES

Other Prediction Methods

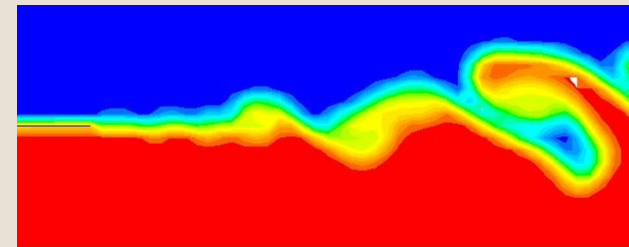
- Different approaches to make turbulence computationally tractable:
 - DNS: Direct Simulation.
 - RANS: Reynolds average (or time or ensemble)
 - LES: Spatially average (or filter)



DNS,
3D unsteady



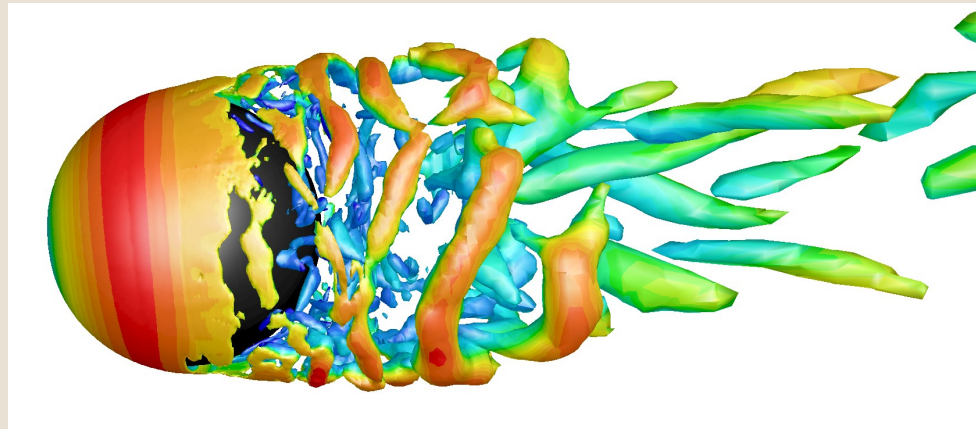
RANS, 2D or 3D
steady or unsteady



LES,
3D unsteady

Why LES?

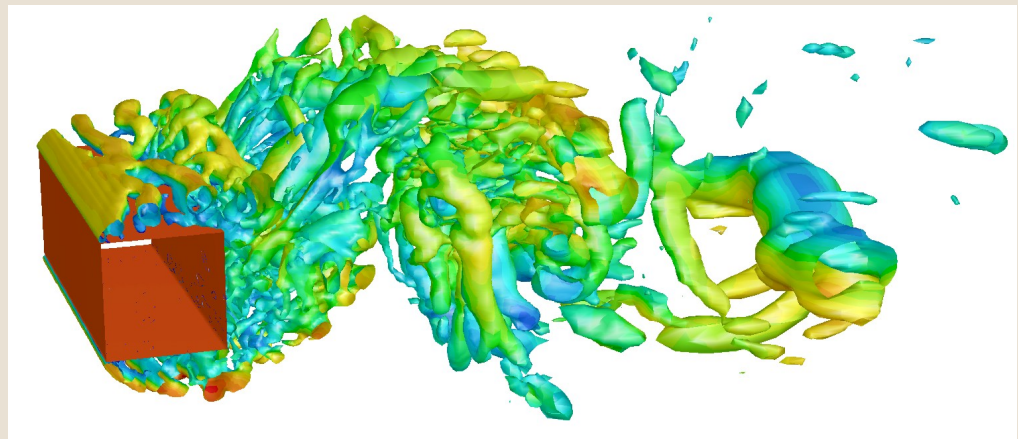
- Some applications need explicit computation of unsteady fields.
 - Bluff body aerodynamics
 - Aerodynamically generated noise (sound)
 - Fluid-structure interaction
 - Combustion instability
 - ...
 - ...



Why LES? - Examples

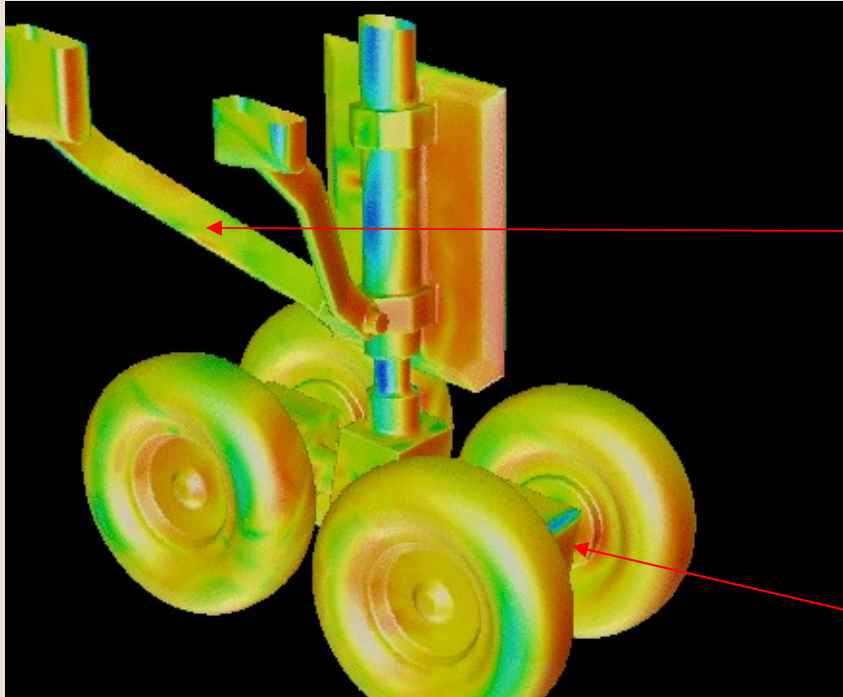
Bluff-Body Aerodynamics

- Unsteadiness in the flow due to large eddies (e.g., unsteady separation, vortex shedding) potentially impacts:
 - Maneuverability (handling quality) of vehicles
 - Safety & comfort (wake of buildings and ships)
 - Unsteady loading on structures (r.m.s. forces and moments, frequency contents)
 - Buildings
 - Bridges

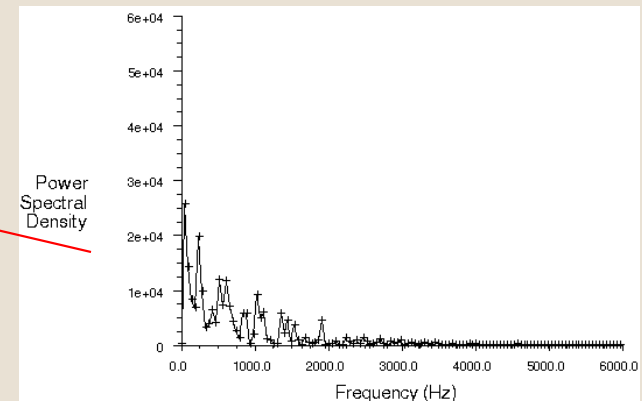
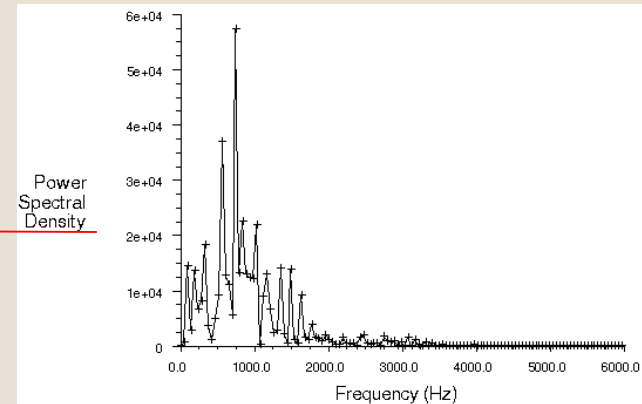


Why LES? – Examples Aerodynamic Noise

- Flow unsteadiness is the very source of aerodynamic noise.

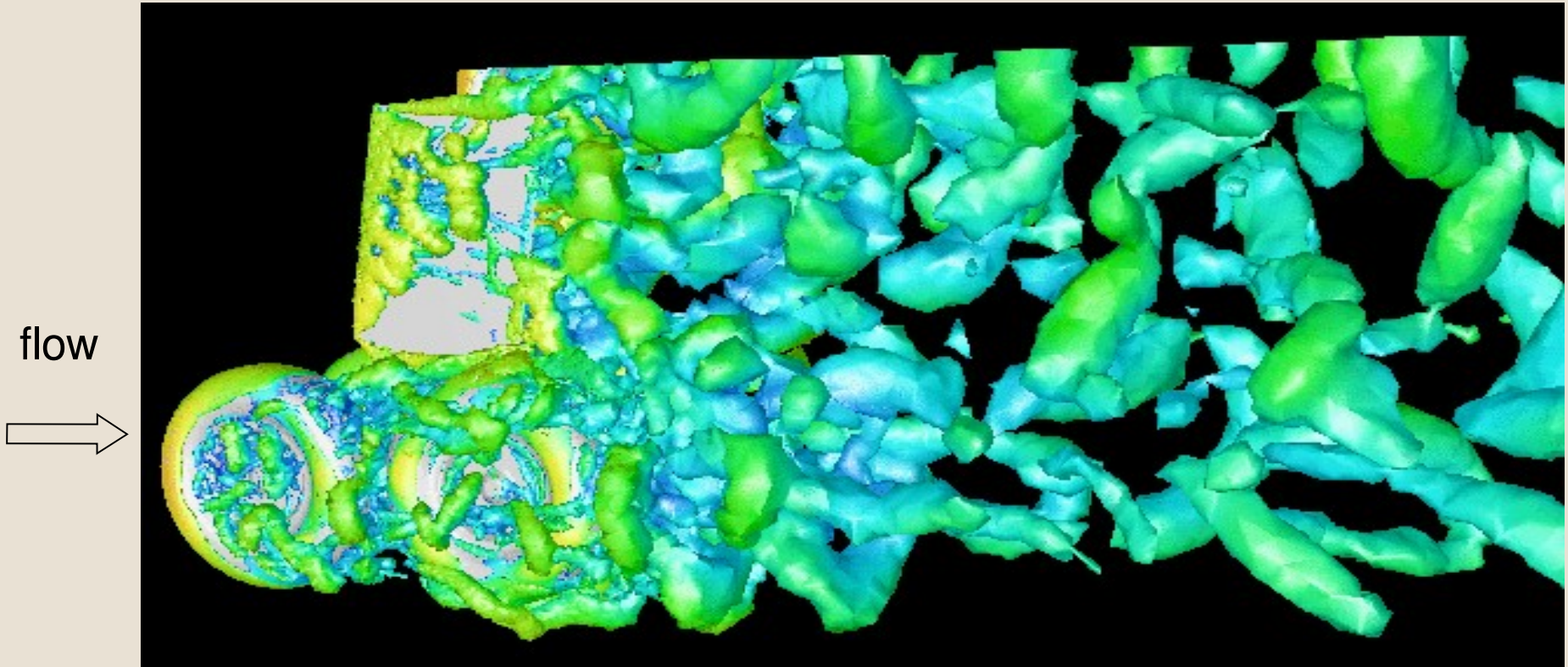


Contours of surface pressure on a
landing gear



PSD of surface static pressure

Why LES? - Examples Aerodynamic Noise – cont'd

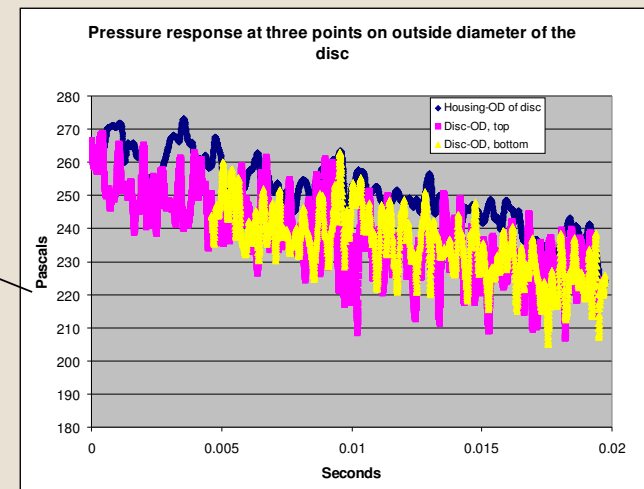
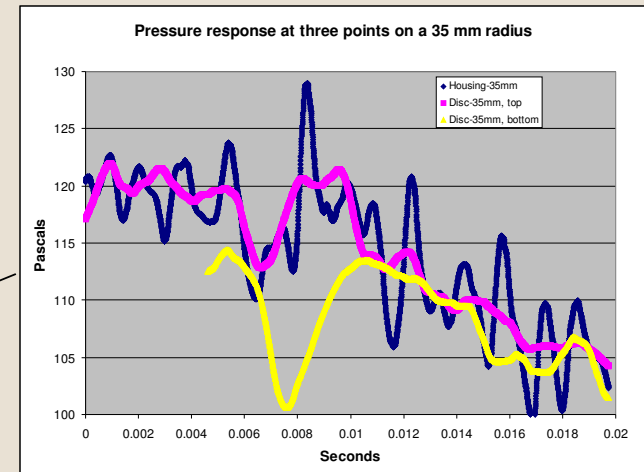
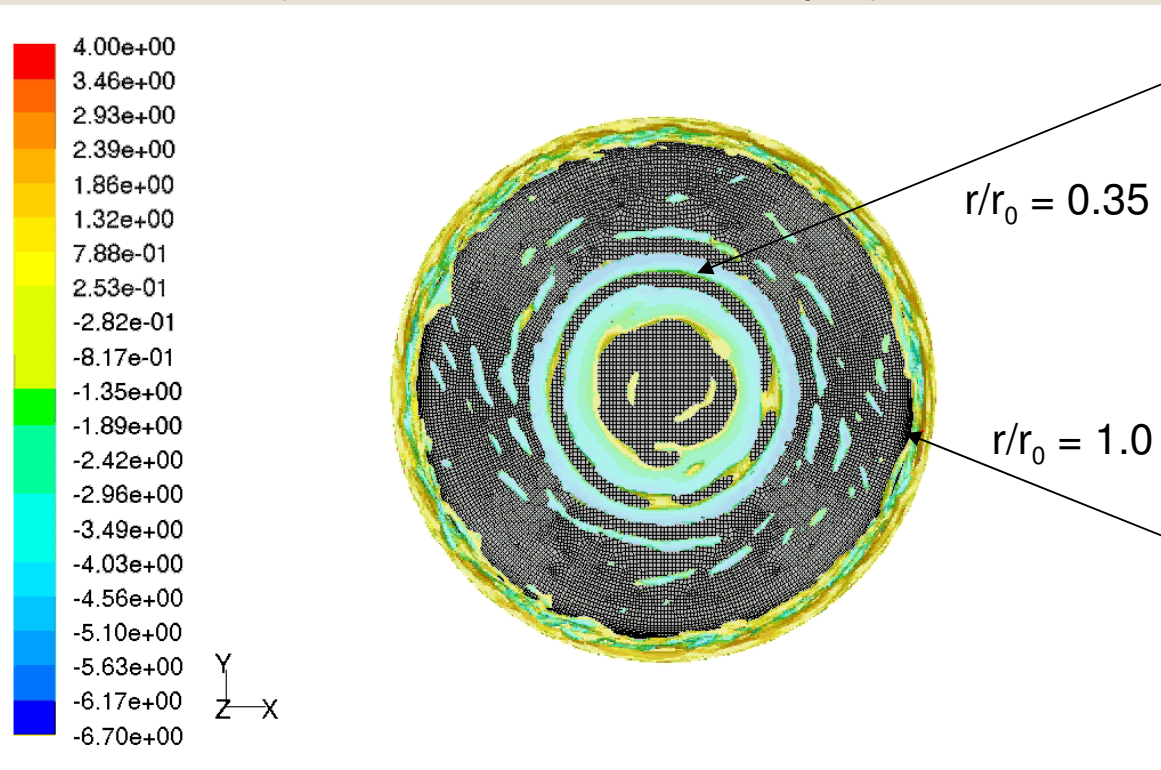


Iso-surface of the second-invariant of the deformation tensor
on a landing gear

Why LES? – Examples Fluid/Structure Interaction

- Unsteady fluid-dynamic loading causes dynamic response of structures

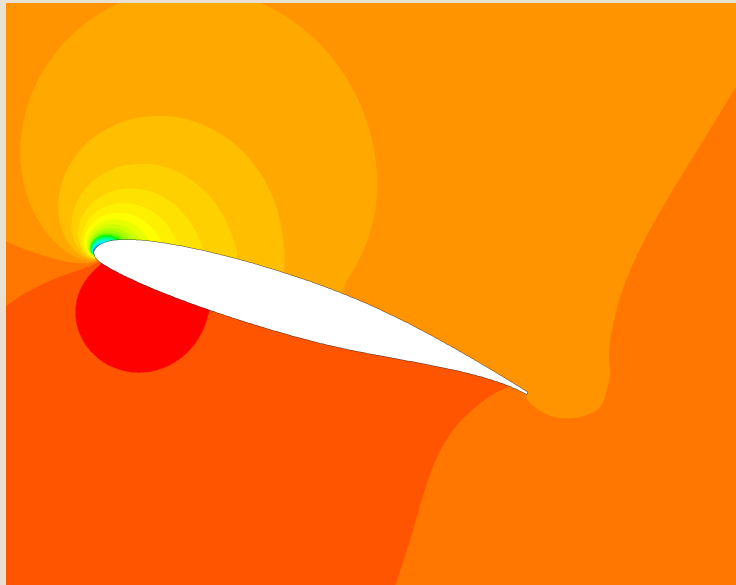
Spinning disk inside a cylindrical enclosure
(D = 95mm, N = 10,000 rpm)



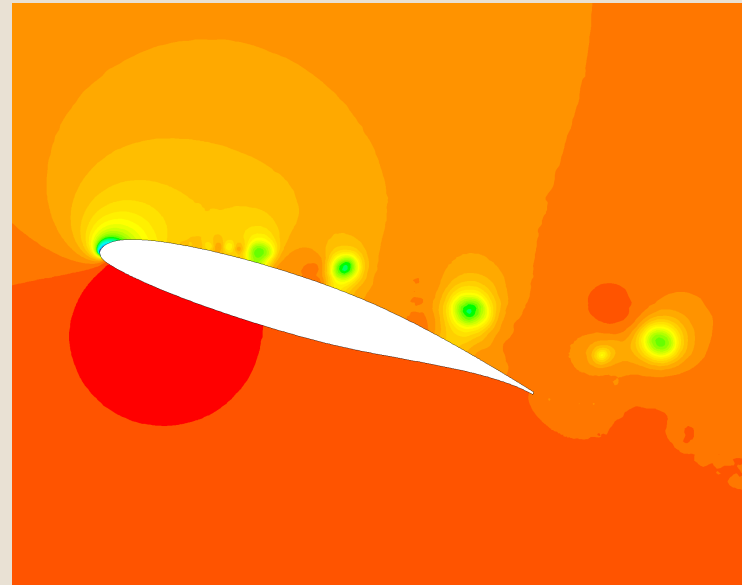
Why LES?

Why Not Unsteady RANS?

- URANS with “good” turbulence models can occasionally predict a regular vortex-shedding (“largest” scale), offering essentially VLES.
- Yet URANS fall sort of capturing the remaining large scales.



URANS with SST $k-\omega$ model



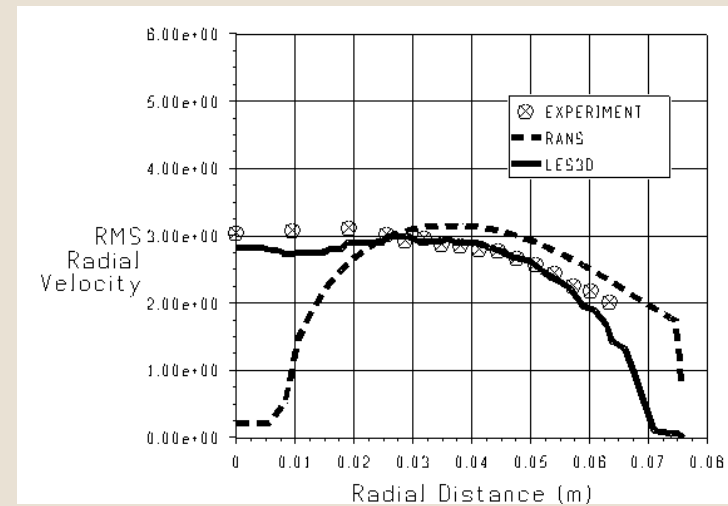
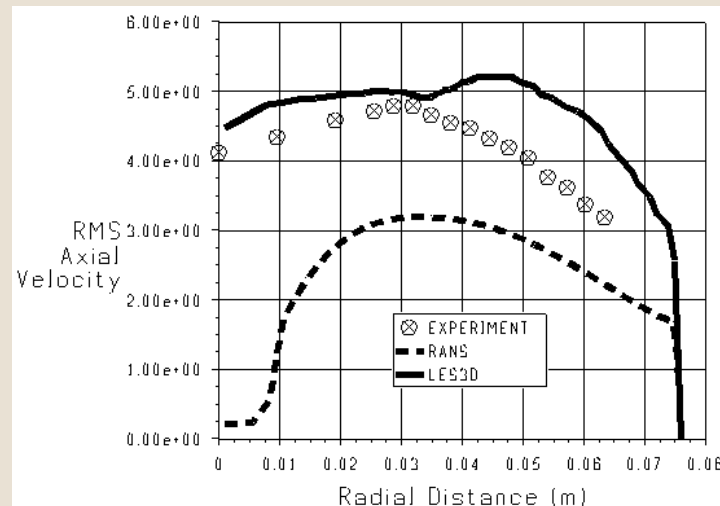
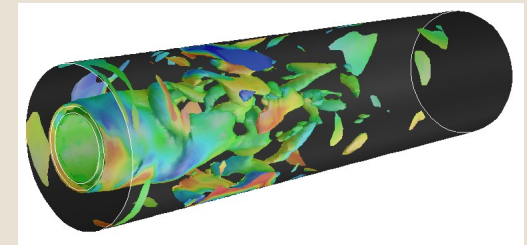
LES

Why LES?

Difficulties with RANS (1)

- RANS-based models often fail to predict even time-averaged quantities.
 - Inability to model the physics of large-scale structures in transporting momentum and scalars

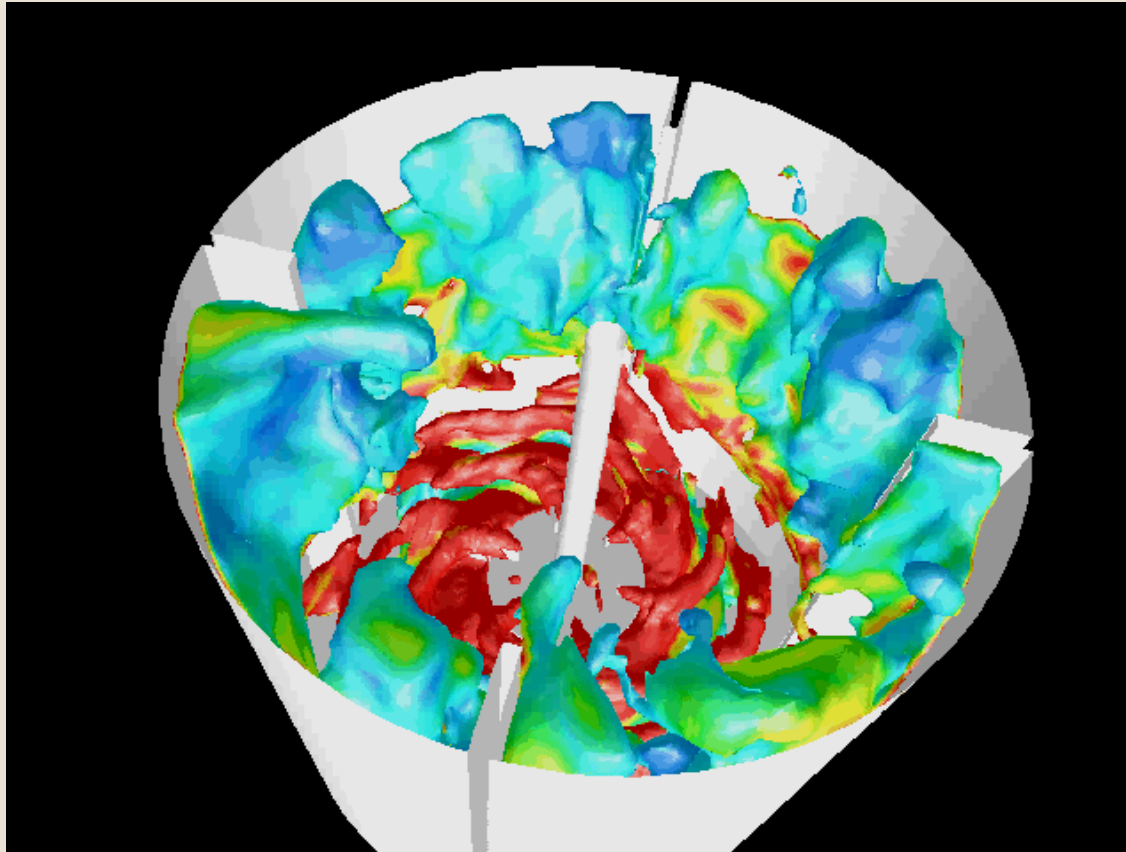
Dump combustor
($Re_D = 10,000$)



Why LES?

Difficulties with RANS (2)

- Large-scale structures mainly contributes to the mixing



Iso-surface of velocity magnitude colored by strain-rate

What About the Cost?

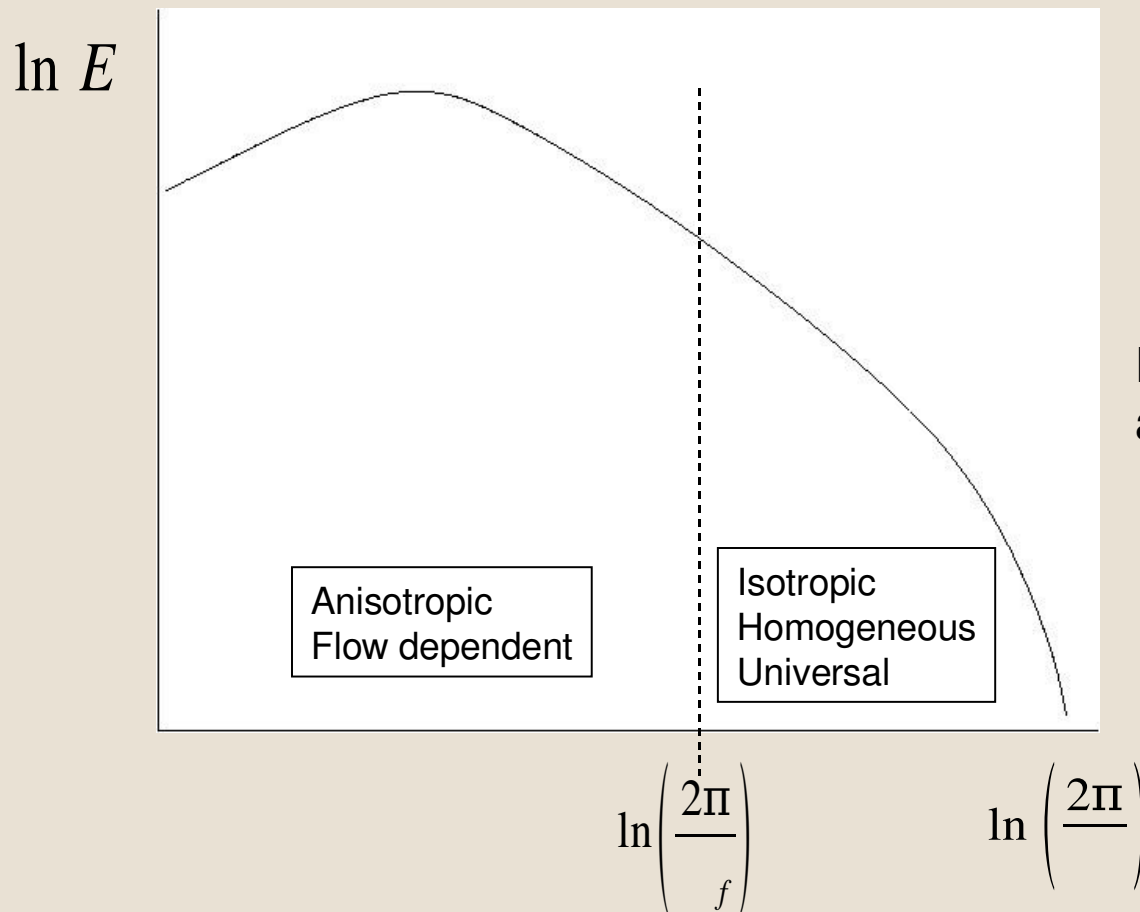
LES is More Expensive



- LES always requires transient 3-D solutions to the filtered N-S equations
- Needs the mesh and the time-step sizes sufficiently fine to resolve the energy-containing eddies
- The cost of resolving near-wall region in high-Re wall-bounded flows is very high
- Compared to DNS ($\sim Re_t^3$), the cost of LES increases much more slowly with Re_t or remains largely independent of Re_t depending on whether or not near-wall region is resolved

What About the Cost? Mesh Resolution (1)

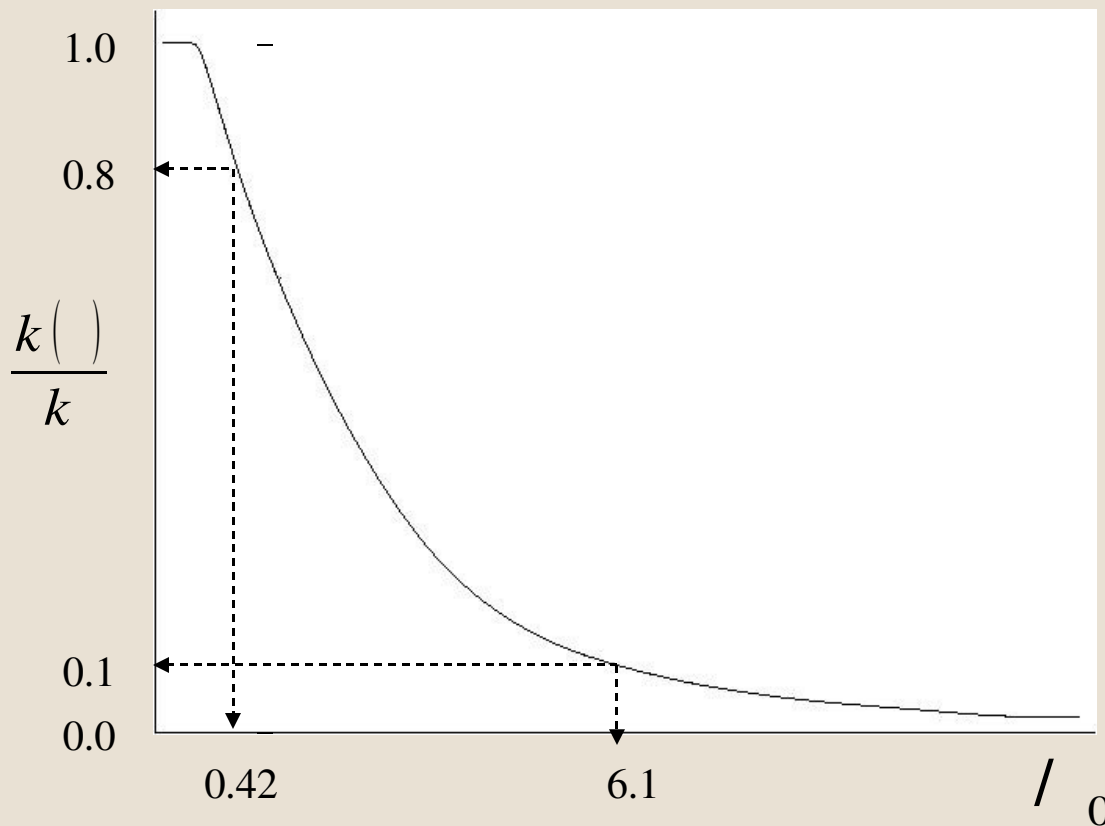
- The mesh resolution determines the fraction of turbulent kinetic energy directly resolved



Energy spectrum
against the length scale

What About the Cost? Mesh Resolution (2)

- Suppose you want to resolve 80% of TKE.
- Then, we need to resolve the eddies whose sizes are larger than roughly half the size of the integral length scale ().



	l/l_0
$k(l) = 0.1 k$	6.10
$k(l) = 0.5 k$	1.6
$k(l) = 0.8 k$	0.42
$k(l) = 0.9 k$	0.16

Cumulative TKE against length-scale of eddies based on the Kolmogorov's energy spectrum

What About the Cost? Time-Step Size

- The time-step size, Δt , should be small enough to resolve the time-scale, τ , of the smallest resolved eddies
- As $\tau \sim \Delta x / U$, it correspond to approximate value of Courant numer $CFL = 1$ (where U is the velocity scale of the flow)

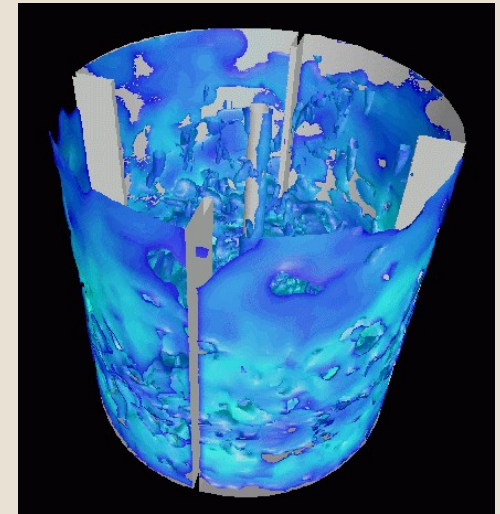
$$CFL = \frac{U \Delta t}{\Delta x} \approx 1.0 \quad \Rightarrow \quad \Delta t = \frac{\Delta x}{U}$$

- **New in 6.2: CFL post-treatment**

What About the Cost? An Example

Lab-scale mixing tanks

- Tank dimension : $L = 300 \text{ mm}$
- Integral length scale $l_0 \sim L/5 \sim 60 \text{ mm}$
- Suppose you have a 100^3 cell mesh
 - This gives an average cell size of $\Delta x = 3 \text{ mm}$.
 - $l_0 = 20 \Delta x$



What About the Cost?

Wall-Bounded Flows (Pope, 2000)

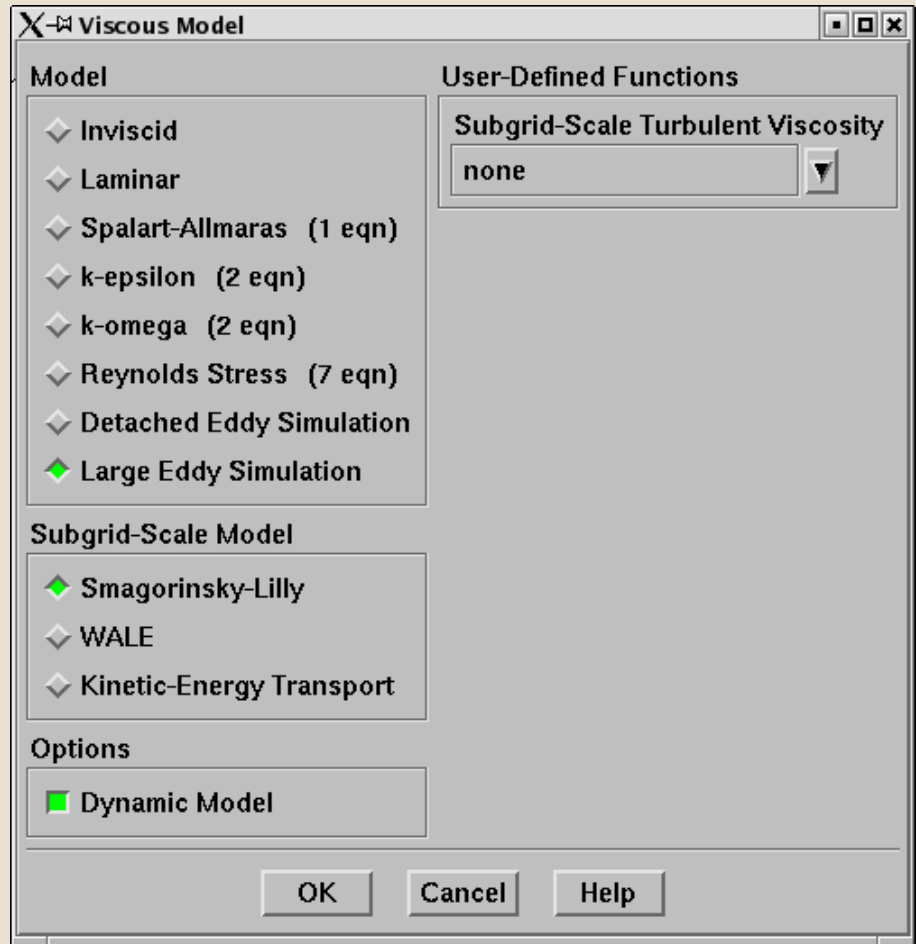


- “Near-wall resolving” approach
 - Turbulence length scale becomes smaller in near-wall region.
 - Resolving the bulk of the energy requires a very fine mesh near the wall.
 - The cost increases as a power of the Reynolds number.
 - Too expensive for high-Re wall-bounded flows
- “Near-wall modelling” approach – An Alternative
 - Wall functions (e.g., laws-of-the-wall)
 - Zonal RANS/LES hybrid approaches (e.g., DES)

What Does FLUENT Offer?

LES Capability in FLUENT

- Underpinnings
 - Numerics
 - SGS turbulence models
 - Post-processing
- FLUENT's LES capability aimed at
 - Accuracy
 - Efficiency
 - Robustness
 - Usability



LES Capability in FLUENT

Numerics - Spatial Discretization (1)



- Spatial accuracy has been greatly improved in recent releases.
 - Major upgrades
 - Node-based gradient scheme (6.1)
 - High-order reconstruction of “convecting” velocity (6.2)
 - Benefits mostly the cases involving unstructured (tet, hybrid) meshes
- Numerical diffusion ought to be minimized in LES.
 - Remember we set out to resolve eddies.
 - RANS vs. LES

$$\mathcal{D}_{t, \text{RANS}} \gg \mathcal{D}_{t, \text{SGS}}$$

LES Capability in FLUENT

Numerics - Spatial Discretization (2)

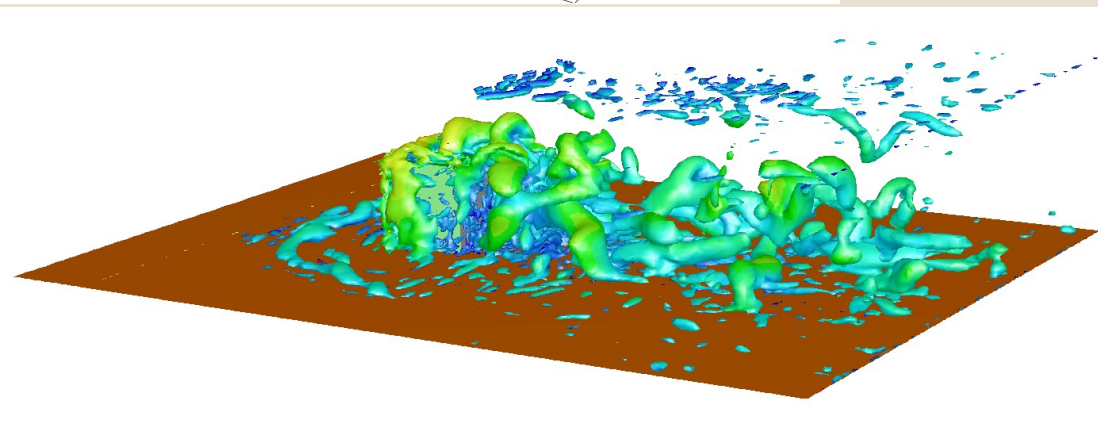
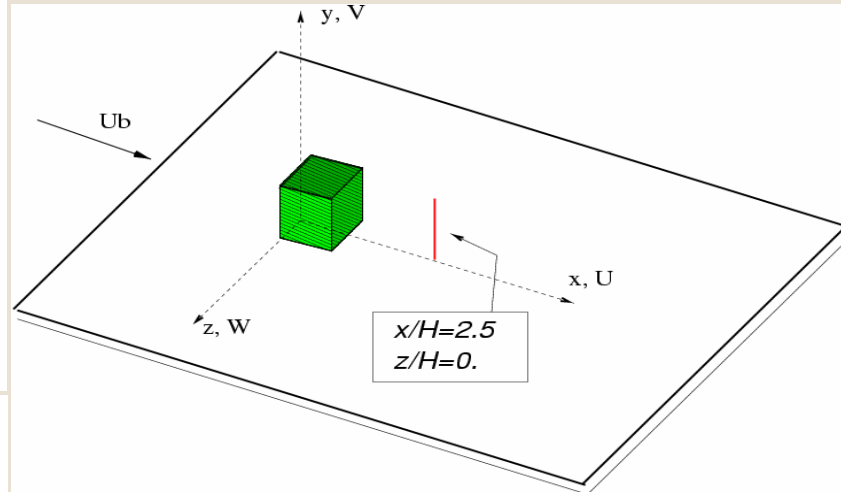
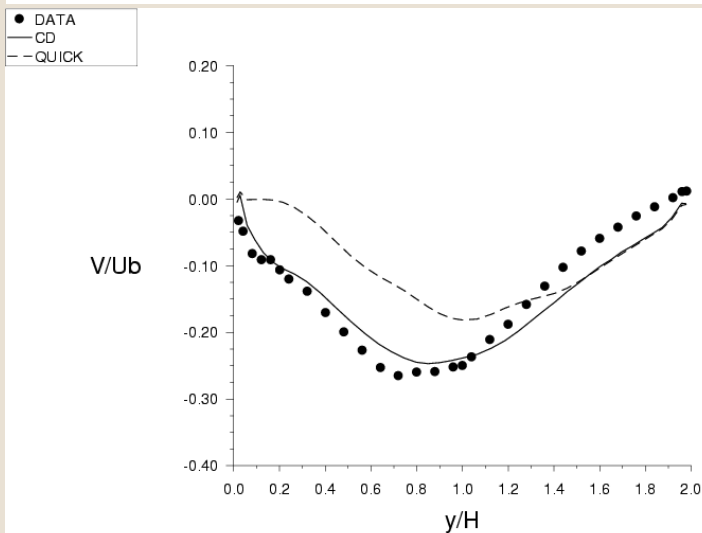
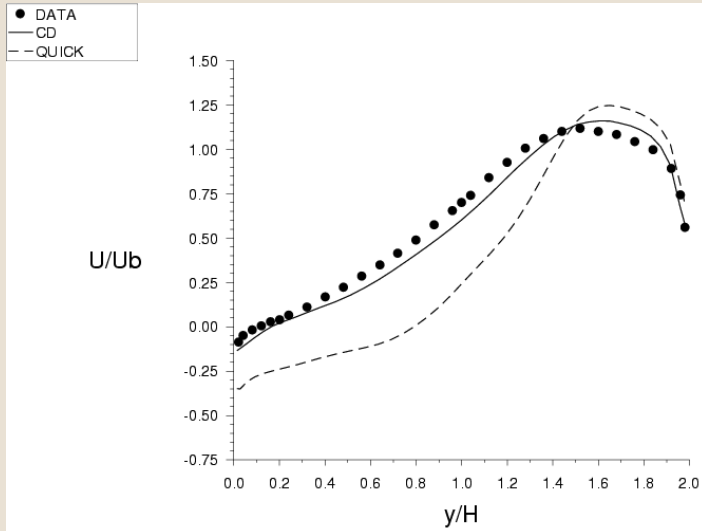


- Discretization of convection terms is the most critical for LES
- FLUENT offers:
 - High-order upwind schemes (SOU, QUICK, MUSCL)
 - Bounded central differencing (BCD) scheme (*new in 6.2, seg. solver only, the default LES-convective scheme in 6.2*)
 - Low-diffusion flux (LDF) scheme (*new in 6.2, coupled solver only, default LES-convective scheme in 6.2*)
 - Central differencing (CD) scheme (*seg. solver only*)
- Central differencing (CD) gives the least numerical diffusion and thus the best accuracy
- Upwind schemes are too diffusive for LES and should be avoided whenever possible

LES Capability in FLUENT

Example: CD vs. QUICK Scheme (1)

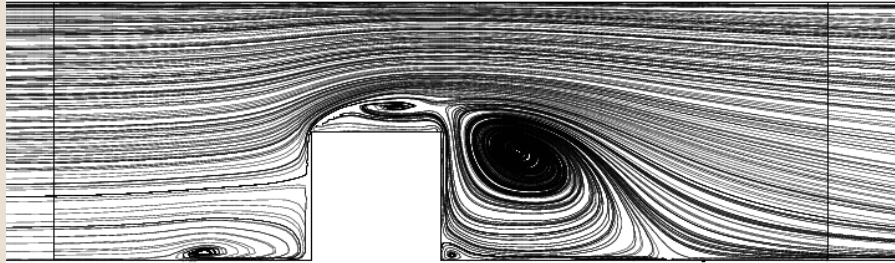
Surface-mounted cube in a channel
(Martinuzzi & Tropea, 1993)



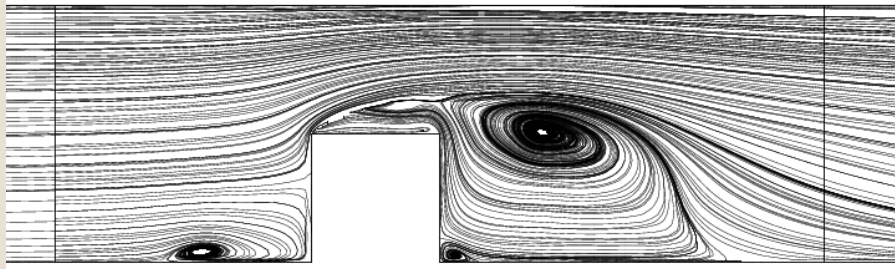
LES Capability in FLUENT

Example: CD vs. QUICK Scheme (2)

Central-differencing



QUICK



Time-averaged streamlines on the mid-plane

Separation and reattachment points predicted by FLUENT and others

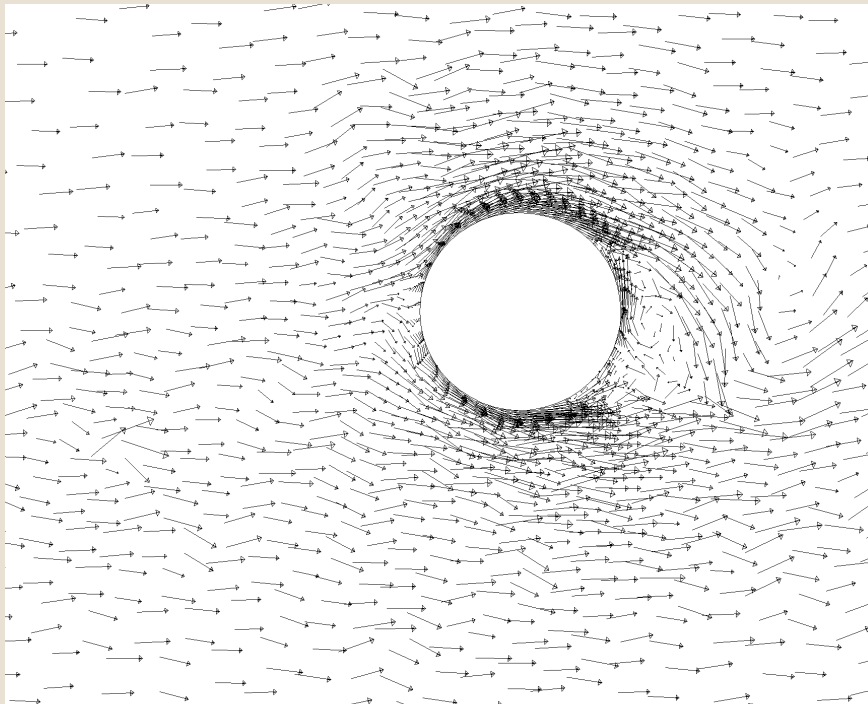
	X_F	X_R
Exp. data (Martinuzzi & Tropea (1993))	1.04	1.61
FLUENT (LES + CD)	1.18	1.78
FLUENT (LES + QUICK)	1.26	2.40
Breuer <i>et al.</i> LES	1.23	1.70

LES Capability in FLUENT

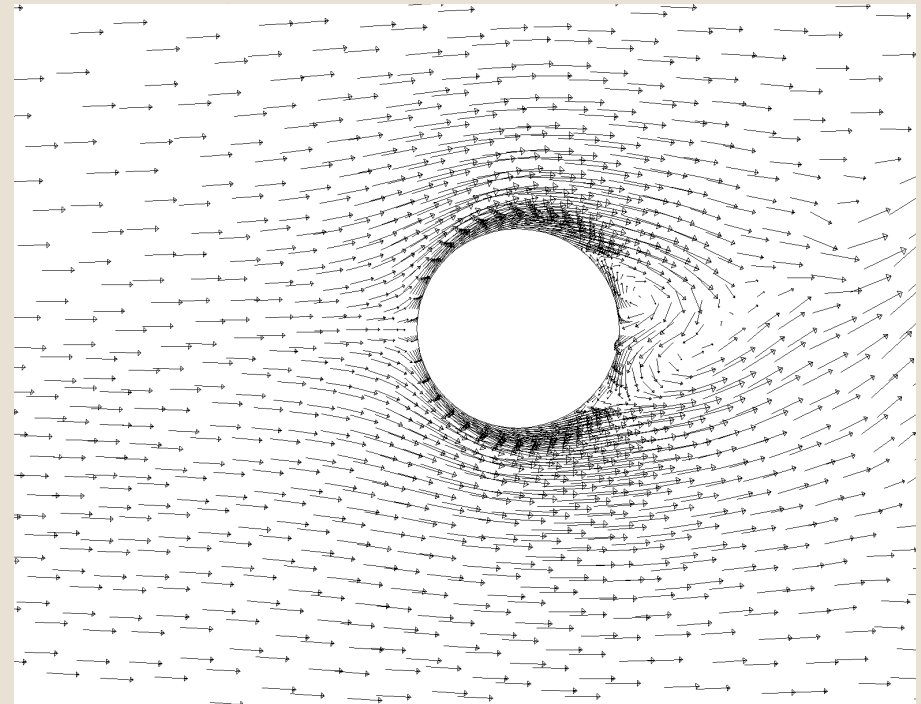
Numerics - Spatial Discretization (3)

- The CD scheme can become unstable, giving unphysical oscillations (wiggles) for high-Re flows.
- The BCD scheme detects and removes the wiggles.

Flow around 2-D section of a landing gear



central differencing

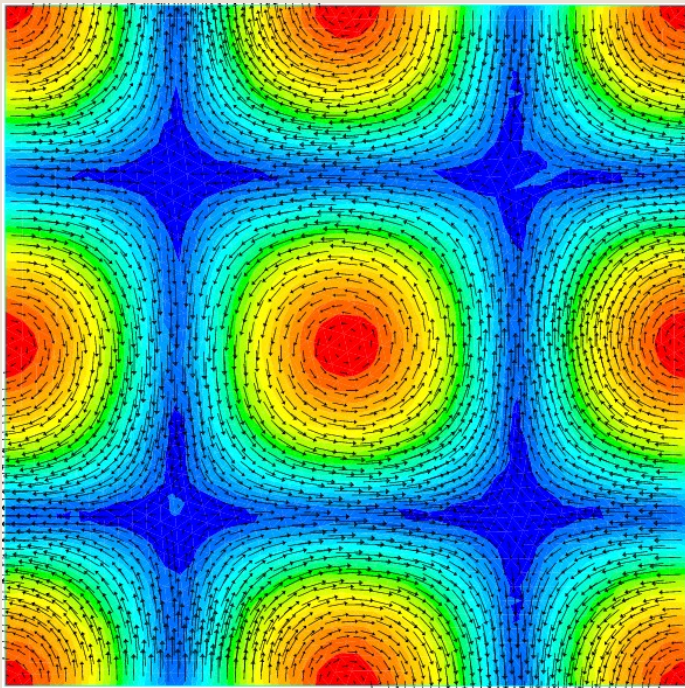


bounded central differencing

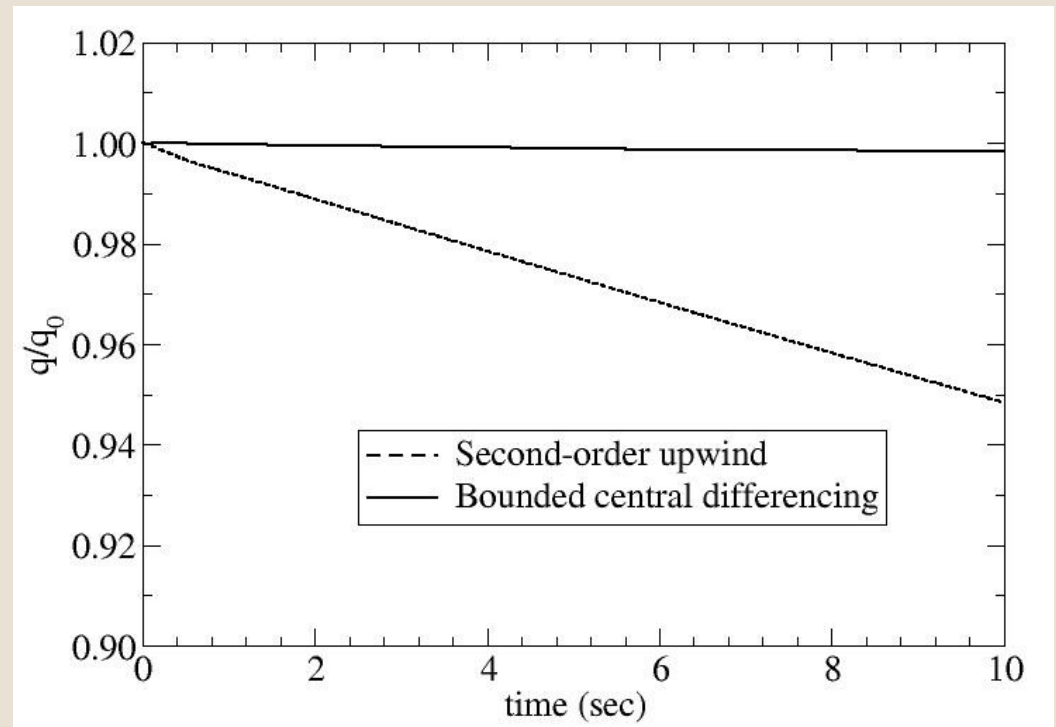
LES Capability in FLUENT

Numerics - Spatial Discretization (4)

- The BCD scheme has much lower numerical diffusion than high-order upwind schemes.



Taylor's inviscid vortex flow –
2-D periodic array of vortices

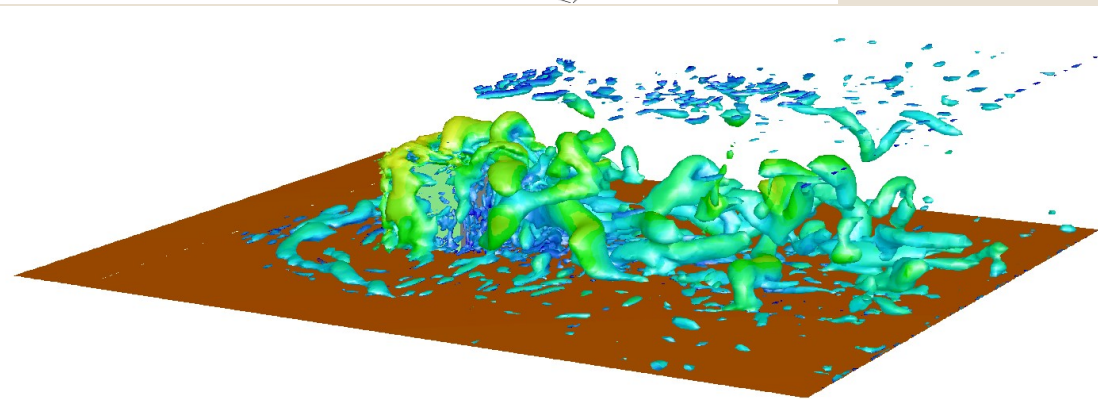
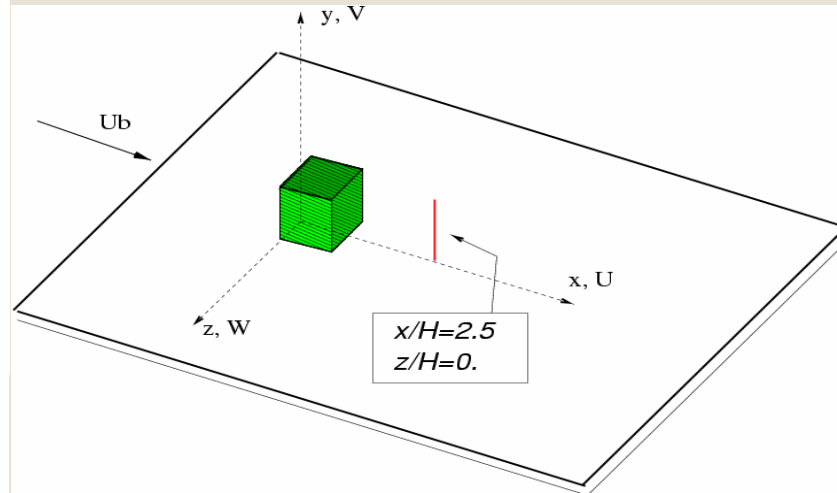
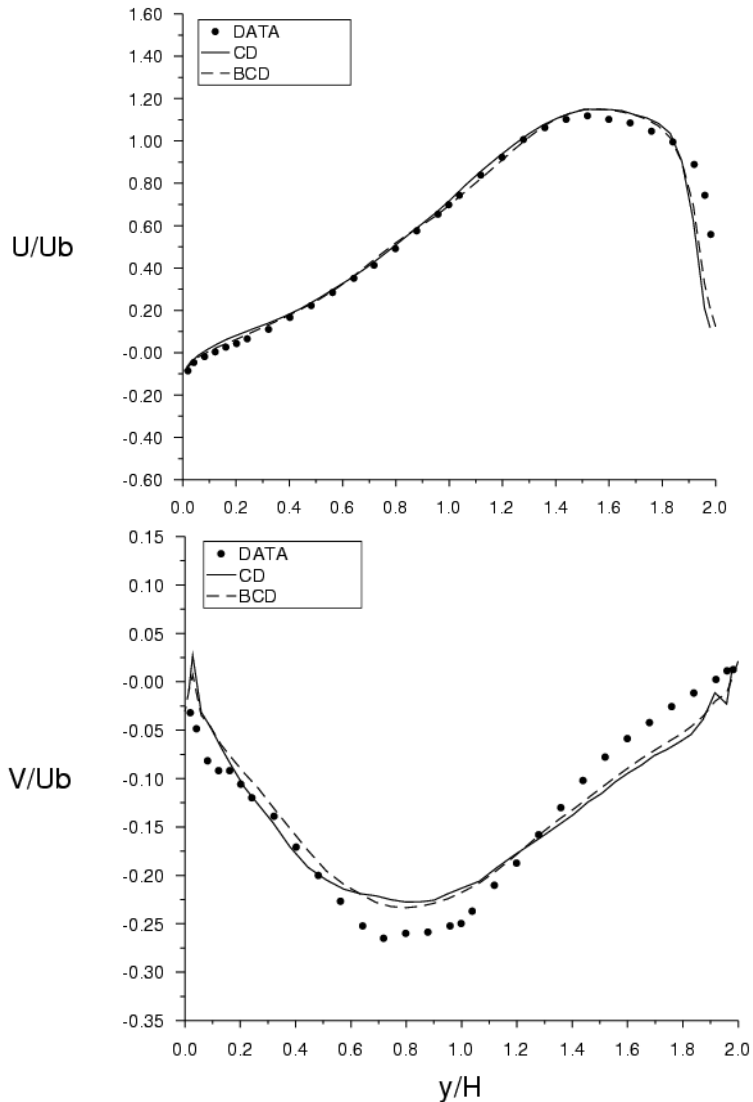


Evolution of total kinetic energy

LES Capability in FLUENT

Example: CD vs. BCD

Surface-mounted cube in a channel (Martinuzzi & Tropea, 1993)



LES Capability in FLUENT

Numerics- Transient Algorithm (1)



- Iterative Time-Advancement (ITA) schemes
 - Has been the workhorse for unsteady flow calculations in FLUENT segregated solver
 - No splitting error
 - Costly due to many outer (velocity-pressure) iterations
 - SIMPLE, SIMPLEC, PISO
- Non-Iterative Time-Advancement (NITA) schemes
 - New in 6.2 (*segregated solver only*)
 - Only one outer iteration per time-step
 - Splitting error commensurate with the truncation error ($\sim O(\Delta t^2)$)
 - Two flavours
 - Fractional-step method
 - PISO

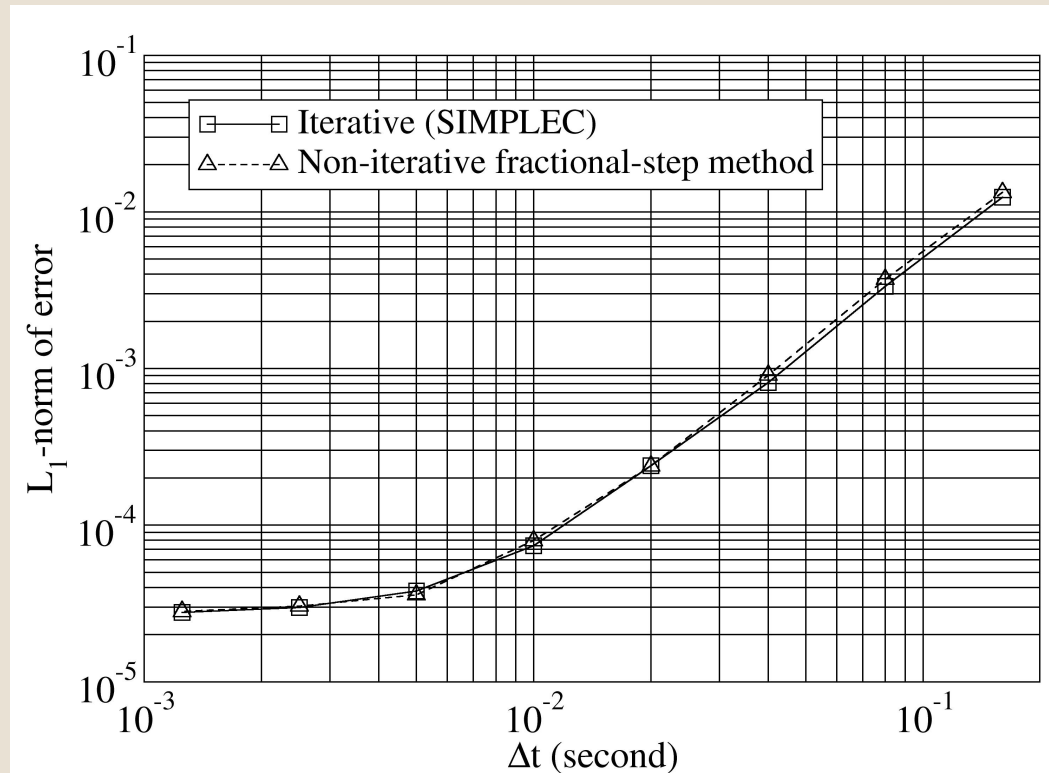
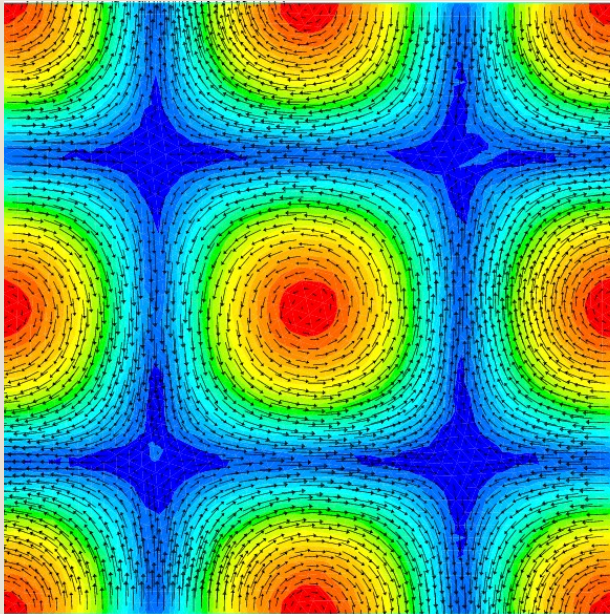
LES Capability in FLUENT

Transient Algorithm (2) – Example

Taylor's Vortex

Comparison of the fully-iterative (SIMPLEC) and non-iterative time-advancement schemes

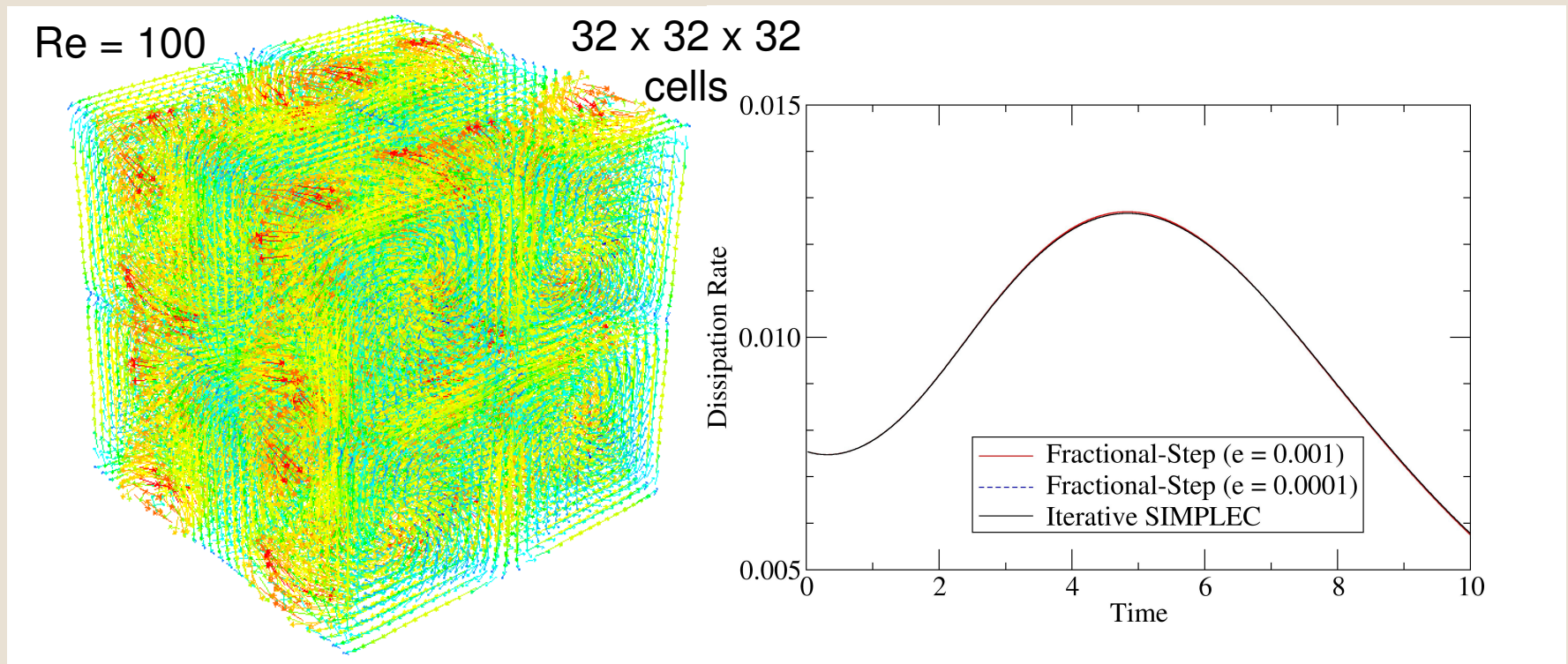
Re = 1



LES Capability in FLUENT Transient Algorithm (3) – Example

Green's Vortex

Comparison of NITA (SIMPEC) and NITA/FSM schemes



Dissipation rate integrated over the volume

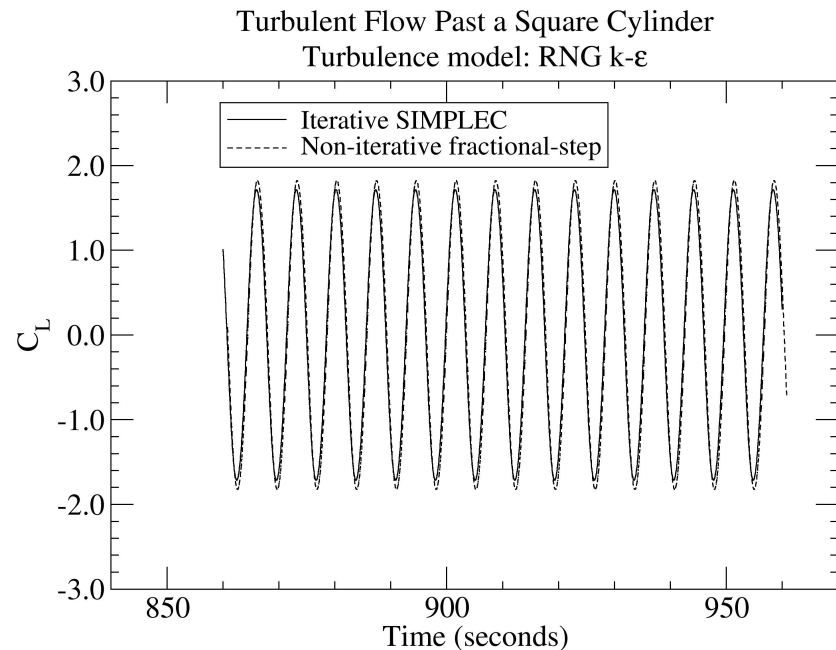
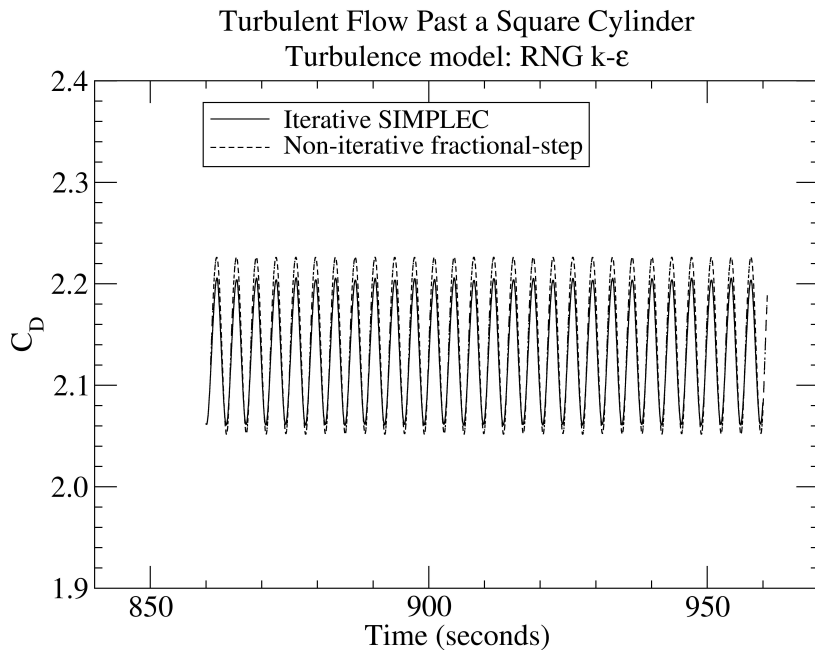
LES Capability in FLUENT

Transient Algorithm (4) – Example

Vortex-Shedding from a Square Cylinder

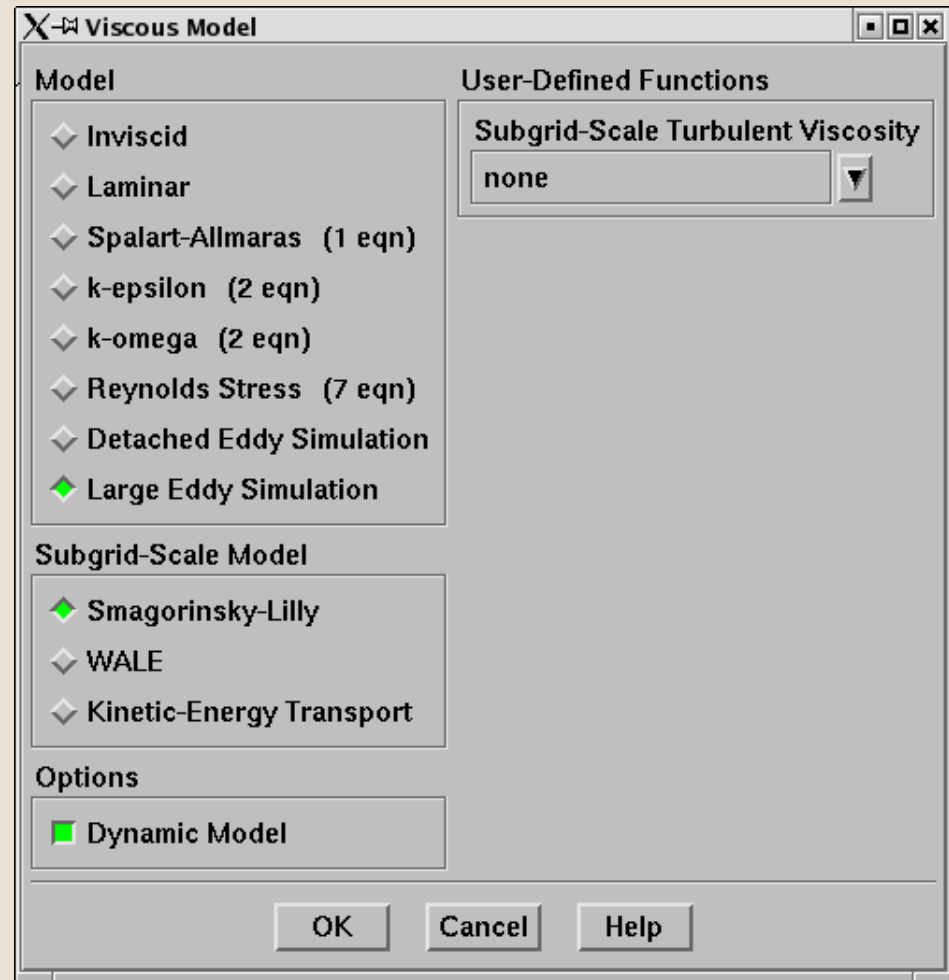
Comparison of NITA (SIMPLEC) and NITA/FSM scheme

$Re_H = 22,000$ (Lyn, 1995), RNG k- ϵ model



LES Capability in FLUENT Subgrid-Scale (SGS) Viscosity Models

- FLUENT 6.2 offers
 - Smagorinsky's model
 - WALE model (new in 6.2)
 - Dynamic Smagorinsky model (new in 6.2)
 - Dynamic subgrid kinetic energy transport model (new in 6.2)



Smagorinsky's Model

- Simple algebraic (0 - equation) model

$$\tau_{ij} - \frac{1}{3} \tau_{kk} \delta_{ij} = -2 \left(C_s \bar{\Delta} \right)^2 |\bar{S}| \bar{S}_{ij}$$

$$\text{with } \bar{\Delta} = \nabla^{1/3}, \quad \bar{S} \equiv \sqrt{2 S_{ij} S_{ij}}$$

- $C_s = 0.1 \sim 0.2$
- The major shortcoming is that there is no C_s universally applicable to different types of flow
- Difficulty with transitional (laminar) flows
- An *ad hoc* damping is needed in near-wall region

WALE Model

- Wall-Adapting Local Eddy-Viscosity model
- Algebraic (0 - equation) model – retains the simplicity of Smagorinsky's model

$$\nu_{SGS} = \left(C_s \right)^2 \frac{\left(S_{ij}^d S_{ij}^d \right)^{3/2}}{\underbrace{\left(\bar{S}_{ij} \bar{S}_{ij} \right)^{5/2} + \left(S_{ij}^d S_{ij}^d \right)^{5/4}}_{\text{near-wall modification}}}$$

- The WALE SGS model adapts to local near-wall flow structure
 - Wall damping effects are accounted for without using the damping function explicitly

WALE Model (cont'd)

- Example

- Simulate the mechanism associated with drag reduction using oscillating walls ($Re_t=395$, $Re_H=20\ 000$)

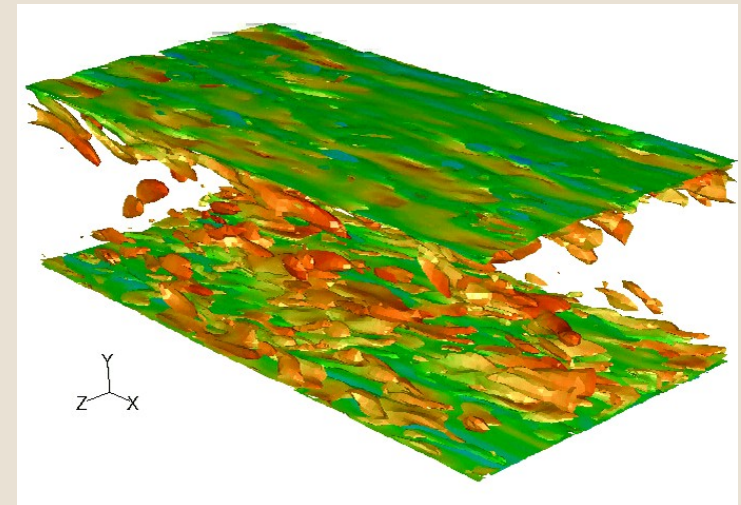
- The wall is forced to oscillate in the span-wise direction with

$$W^+ = A^+ \sin(2\pi t^+/T^+)$$

- Interaction between the stokes layer and the near-wall structures

Reduction rate (%) in wall-shear

	$A^+=5$	$A^+=10$	$A^+=20$
LES (FLUENT)	10.	22.	30.4
DNS (Choi <i>et al</i>)	9.4	22.8	30.6



Dynamic Smagorinsky's Model

- Based on the similarity concept and Germano's identity (Germano *et al.*, 1991; Lilly, 1992)
- The model parameter (C_s) is automatically adjusted using the resolved velocity field
- FLUENT implementation
 - Locally dynamic model
 - Adapted for unstructured meshes (test-filter)
- Overcomes the shortcomings of the Smagorinsky's model
 - Can handle transitional flows
 - The near-wall (damping) effects are taken into account

Dynamic Subgrid KE Transport Model

- Kim and Menon (1997)
- One-equation (for SGS kinetic energy) model

$$\tau_{ij} - \frac{1}{3} \tau_{kk} \delta_{ij} = -2C_k k_{sgs}^{1/2} \bar{S}_{ij}$$

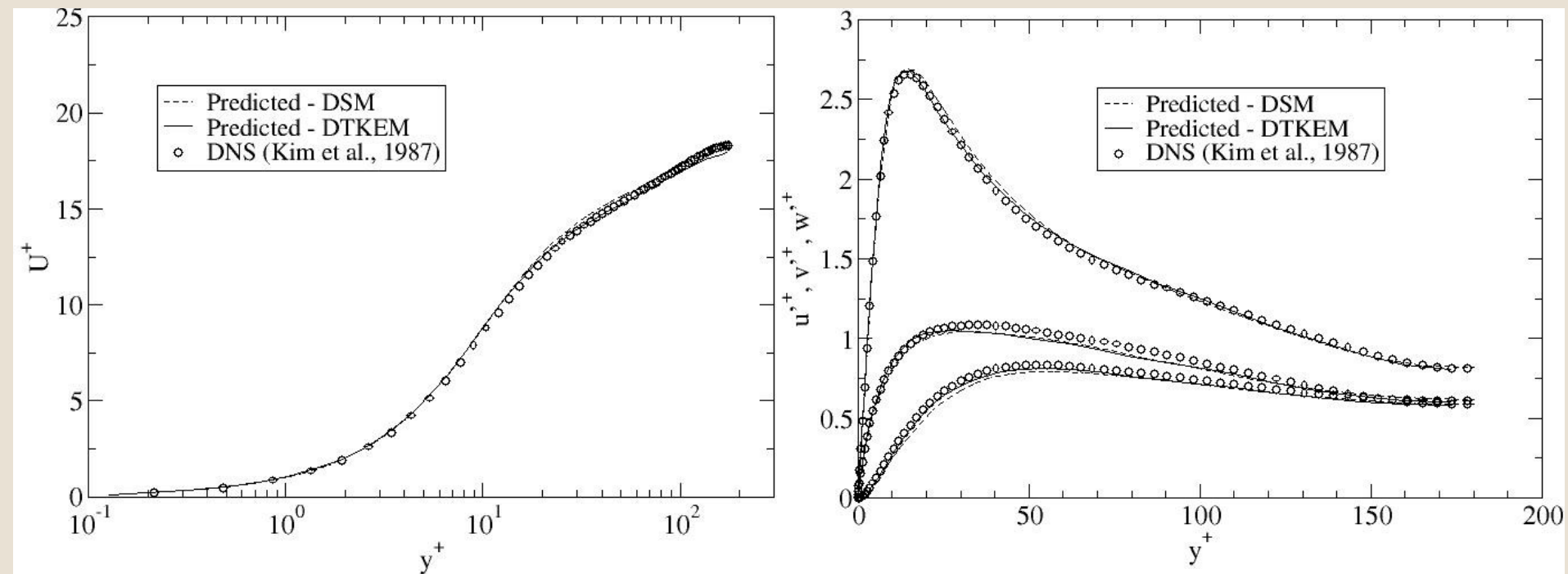
$$\frac{\partial k_{sgs}}{\partial t} + \frac{\partial \bar{u}_j k_{sgs}}{\partial x_j} = -\tau_{ij} \frac{\partial \bar{u}_i}{\partial x_j} - C_\epsilon \frac{k_{sgs}^{3/2}}{\bar{\nu}_{sgs}} + \frac{\partial}{\partial x_j} \left(\frac{\nu_{sgs}}{\sigma_k} \frac{\partial k_{sgs}}{\partial x_j} \right)$$

- Like the dynamic Smagorinsky's model, the model constants (C_k , C_ϵ) are automatically adjusted on-the-fly using the resolved velocity field.
- The dynamic procedure has stronger arguments than the dynamic Smagorinsky's model.

LES Capability in FLUENT Subgrid-Scale (SGS) Viscosity Models

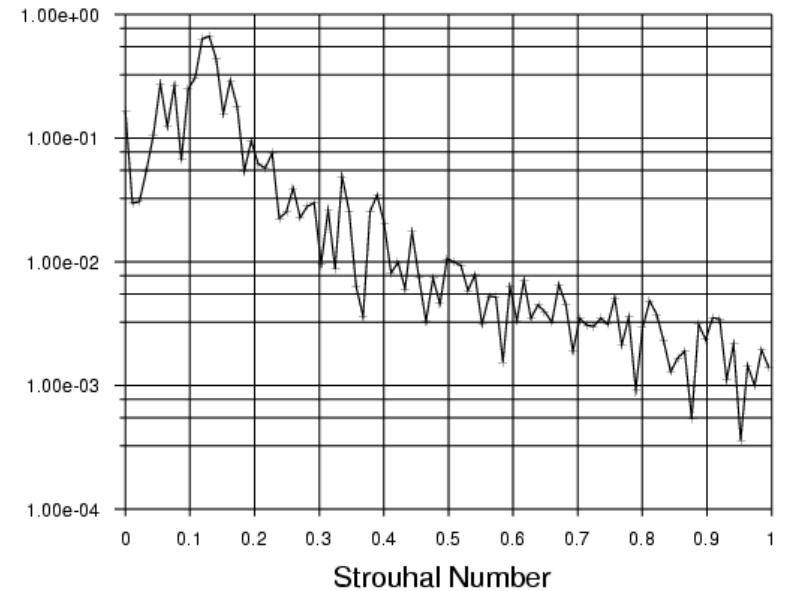
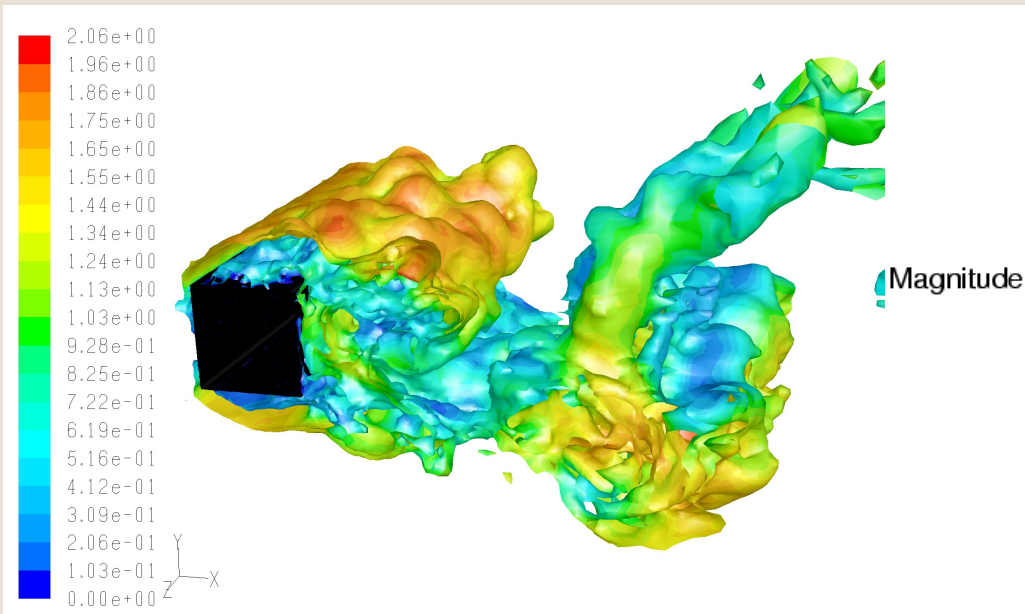
Channel Flow ($Re_t = 180$)

72 x 72 x 72 cells



Example: LES of the Flow Past a Square Cylinder ($Re_H = 22,000$)

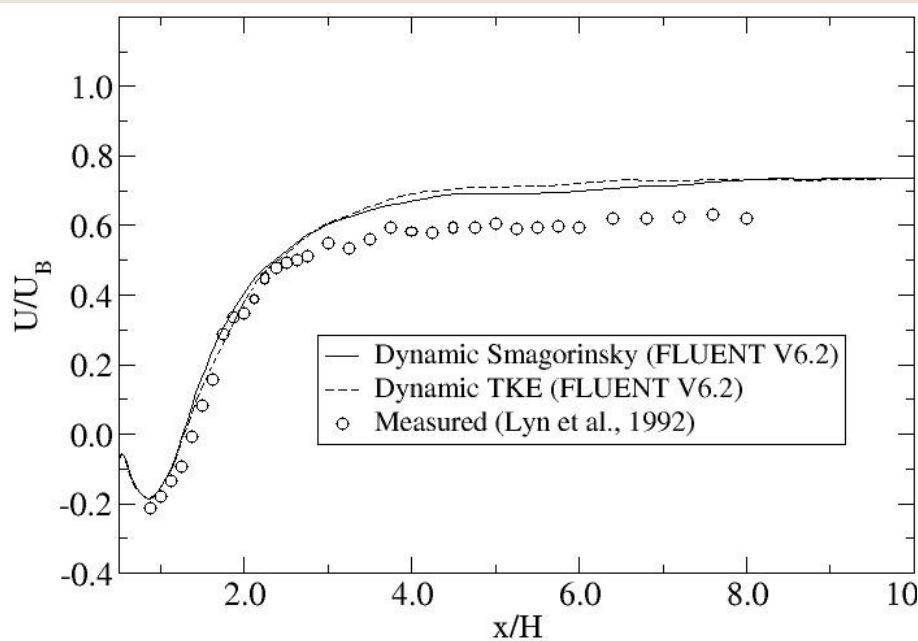
	C_D	St
Dynamic Smag.	2.28	0.130
Dynamic TKE	2.22	0.134
Exp.(Lyn <i>et al.</i> , 1992)	2.1 – 2.2	0.130



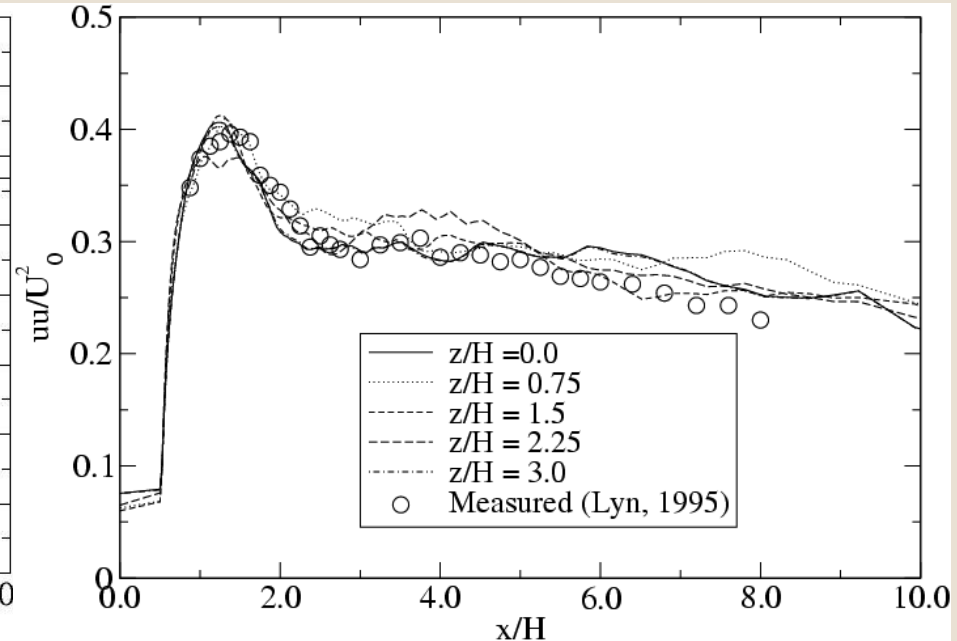
Iso-contours of instantaneous vorticity magnitude

C_L spectrum

Example: LES of the Flow Past a Square Cylinder ($Re_H = 22,000$)



Streamwise mean velocity
along the wake centerline



Streamwise normal stress
along the wake centerline

LES Capability in FLUENT

SGS Models: Summary



Sub-grid stress : turbulent viscosity

- Smagorinsky model (*Smagorinsky, 1963*)
 - Need ad-hoc near wall damping
- WALE model (*Nicoud & Ducros 1999*)
 - Correct asymptotic near wall behaviour
- Dynamic model (*Germano et al., 1991*)
 - Local adaptation of the Smagorinsky constant
- Dynamic sub-grid kinetic energy transport model (*Kim & Menon 2001*)
 - Robust constant calculation procedure
 - Physical limitation of backscatter

$$\tau_{ij} - \frac{1}{3} \tau_{kk} \delta_{ij} = -2\rho v_t \bar{S}_{ij}$$

$$v_t = (C_s \bar{\Delta})^2 |\bar{S}|$$

$$v_t = (C_s \bar{\Delta})^2 \frac{(S_{ij}^d S_{ij}^d)^{3/2}}{(\bar{S}_{ij} \bar{S}_{ij})^{5/2} + (S_{ij}^d S_{ij}^d)^{5/4}}$$

$$v_t = (C_D \bar{\Delta})^2 |\bar{S}|$$

$$v_t = C_k k_{sgs}^{1/2}$$

$$\frac{\partial k_{sgs}}{\partial t} + \frac{\partial \bar{u}_j k_{sgs}}{\partial x_j} = -\tau_{ij} \frac{\partial \bar{u}_i}{\partial x_j} - C_\epsilon \frac{k_{sgs}^{3/2}}{\bar{\Delta}} + \frac{\partial}{\partial x_j} \left(\frac{\nu_{sgs}}{\sigma_k} \frac{\partial k_{sgs}}{\partial x_j} \right)$$

LES Capability in FLUENT

LES for Combustion Simulation

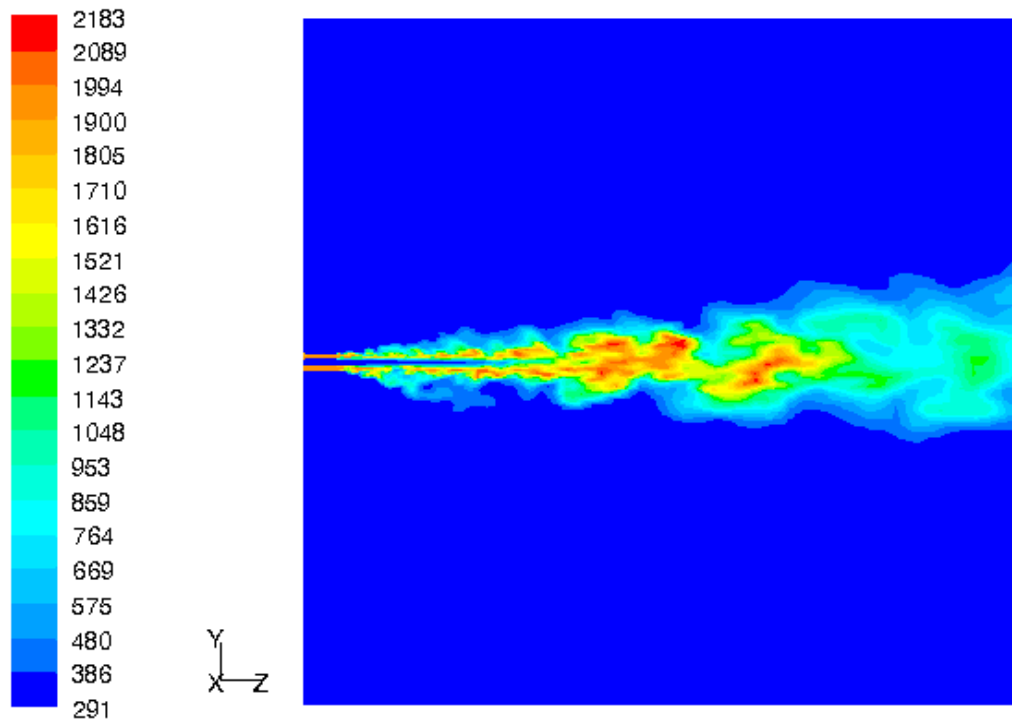


- LES is compatible with all FLUENT's turbulent combustion models
 - Eddy-dissipation/finite-rate
 - Non-premixed combustion model (mixture-fraction/PDF)
 - Partially-premixed or premixed combustion model (Reaction-progress variable)
 - PDF transport
- The dynamic procedure is not implemented yet for scalar transport equations
 - Subgrid-scale turbulent diffusivities are computed with Prandtl (Schmidt) number.

LES Capability in FLUENT

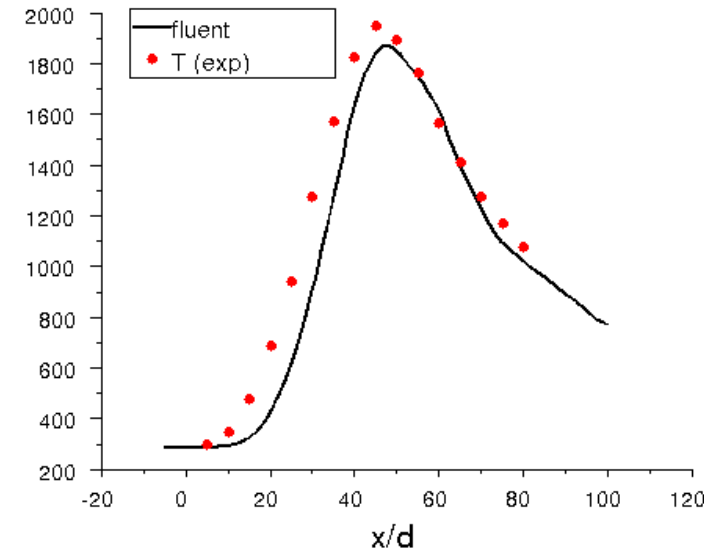
Example: Combustion Simulation

LES for Sandia Flame-D using mixture-fraction/PDF model



Contours of Static Temperature (k) (Time=5.0090e-01) Mar 09, 2004
FLUENT 6.2 (3d, segregated, pdf23, LES, unsteady)

Instantaneous temperature field



Mean temperature (in K) along the centreline

LES Capability in FLUENT Inflow Boundary Conditions



- It is often important to specify a realistic turbulent inflow velocity for accurate prediction of the (downstream) flow

$$u_i(x, t) = \underbrace{U_i(x)}_{\text{time-averaged}} + \underbrace{u_i'(x, t)}_{\text{coherent + random}}$$

- The random-number based inflow boundary condition in 6.1 is superseded by two new methods in 6.2
 - Spectral synthesizer
 - Vortex method

Spectral Synthesizer (1)

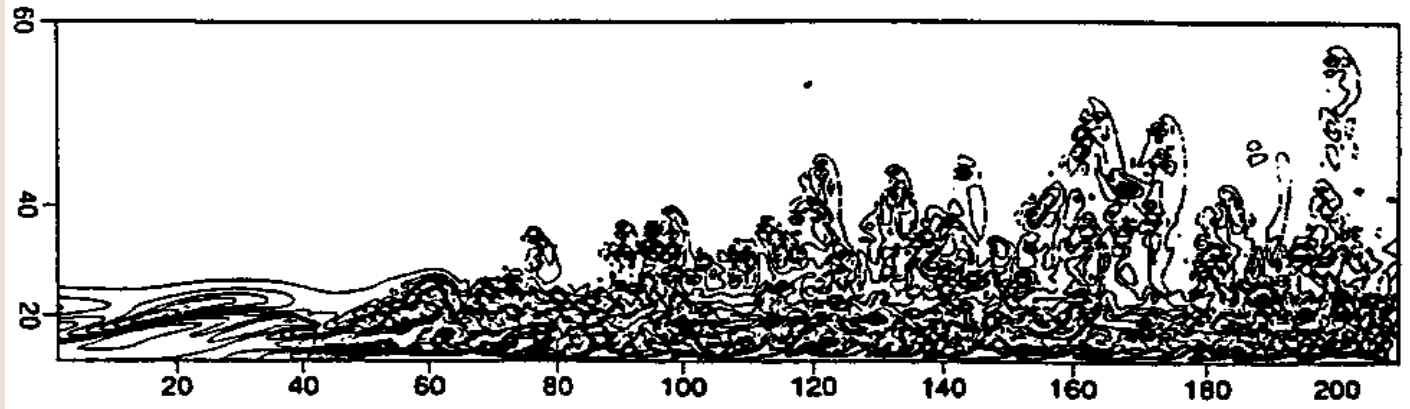
- Largely based on the work of Celik *et al.*(2001)

$$v_i(\vec{x}, t) = \sqrt{\frac{2}{N}} \sum_{n=1}^N [p_i^n \cos(\tilde{k}_j^n \tilde{x}_j + \omega_n \tilde{t}) + q_i^n \sin(\tilde{k}_j^n \tilde{x}_j + \omega_n \tilde{t})]$$

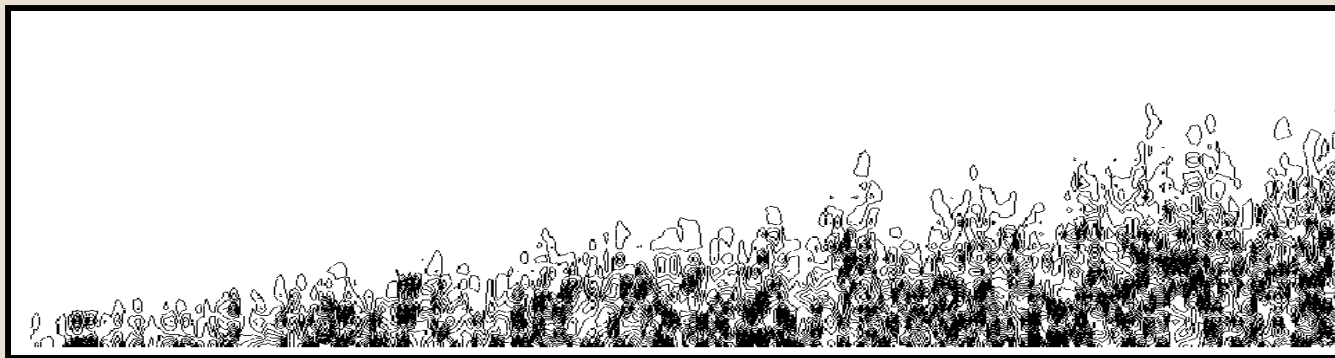
- Able to synthesize anisotropic, inhomogeneous turbulence from RANS results (k - ϵ , k - ω , and RSM fields)
- The velocity-field satisfies the continuity by design.

LES Capability in FLUENT Inflow Boundary and Conditions

Spectral Synthesizer (2)



Speziale, C.G., AIAA J., Vol.36, No.2, 1998



A.Smirnov, I.Celik, S.Shi, JFE, Vol.123, pp.359-371, 2001

Vortex Method

- In essence, vorticity-transport is modeled by distributing and tracking many point-vortices on a plane (Sergent, Bertoglio)

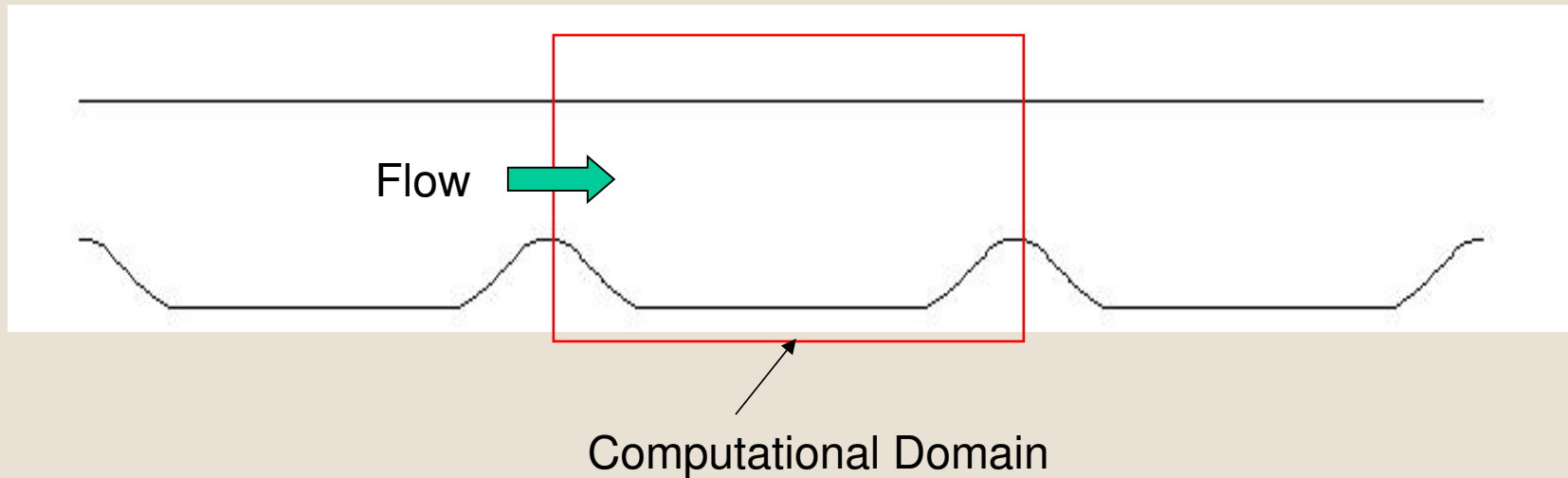
$$\omega(x, t) = \sum_{k=1}^N \Gamma_k(t) \eta(|x - x_k|, t)$$

- Velocity field computed using the Biot-Savart's law

$$u(x, t) = -\frac{1}{2\Pi} \iint \frac{(x - x') \times \omega(x') e_z}{|x - x'|^2} dx'$$

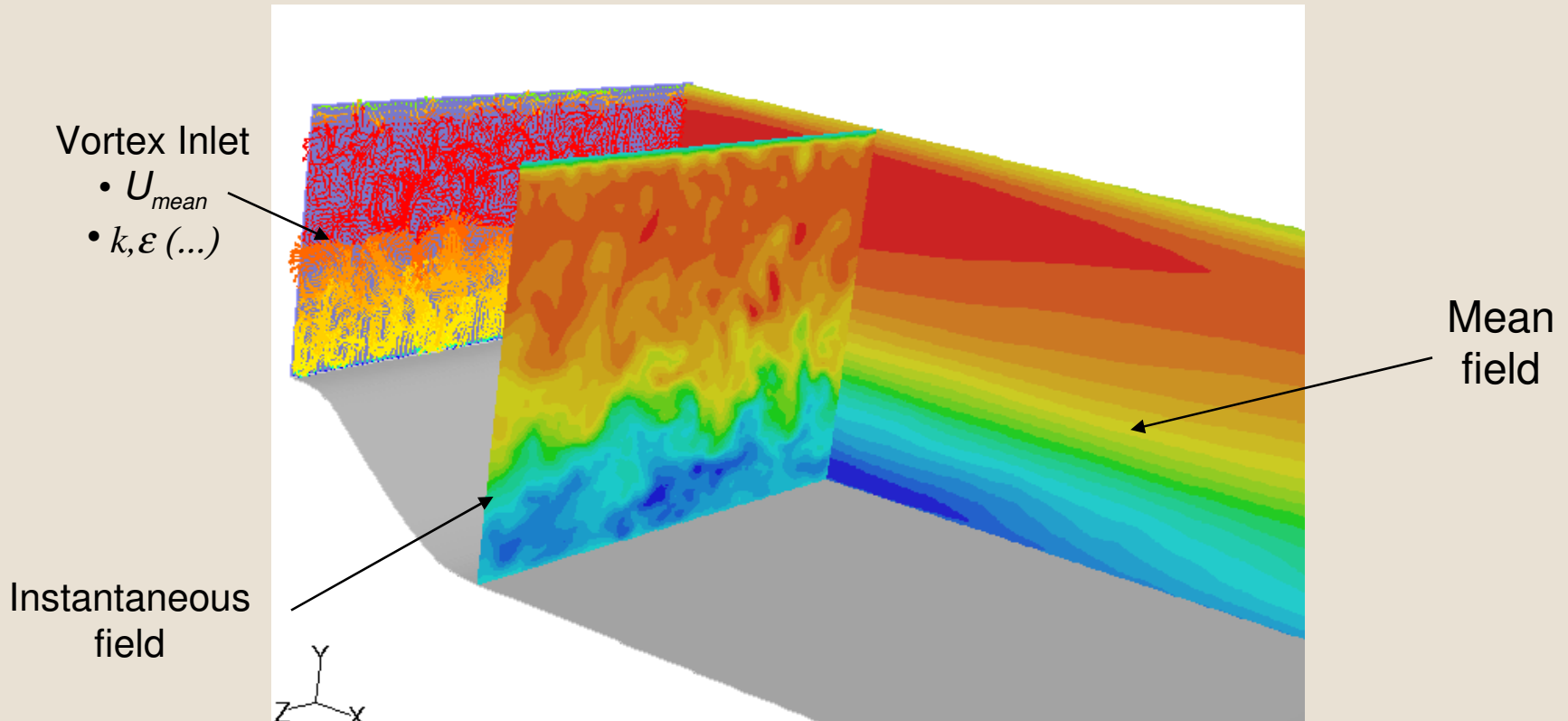
Vortex Method - Example

3-D Wavy Channel ($Re_H = 10,600$)



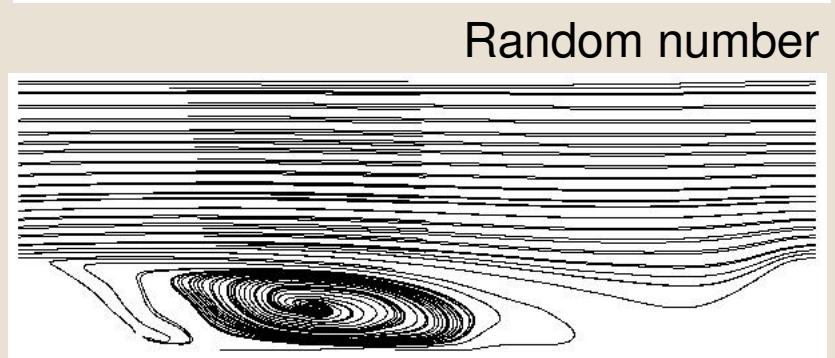
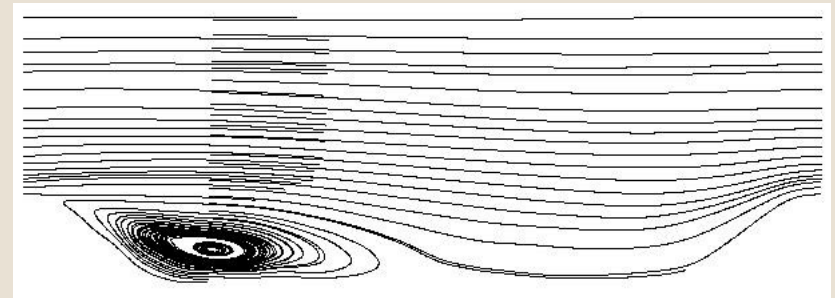
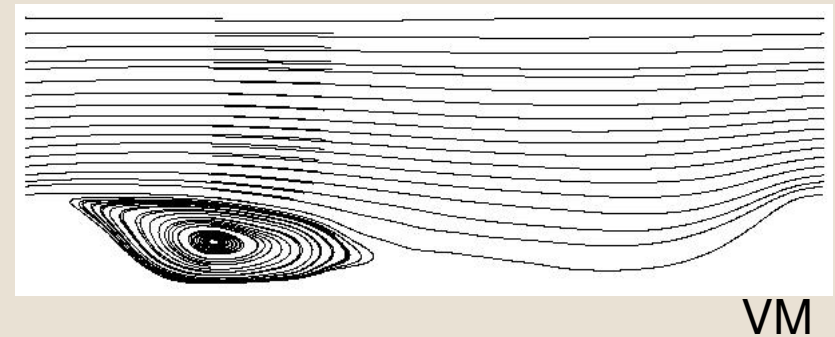
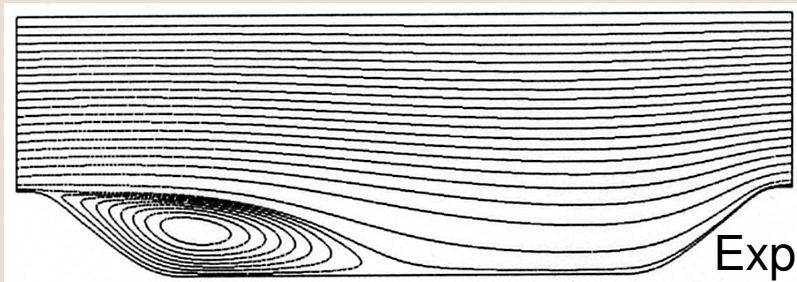
LES Capability in FLUENT Inflow Boundary Conditions

Vortex Method – Example (cont'd)



LES Capability in FLUENT Inflow Boundary Conditions

Vortex Method – Example (cont'd)

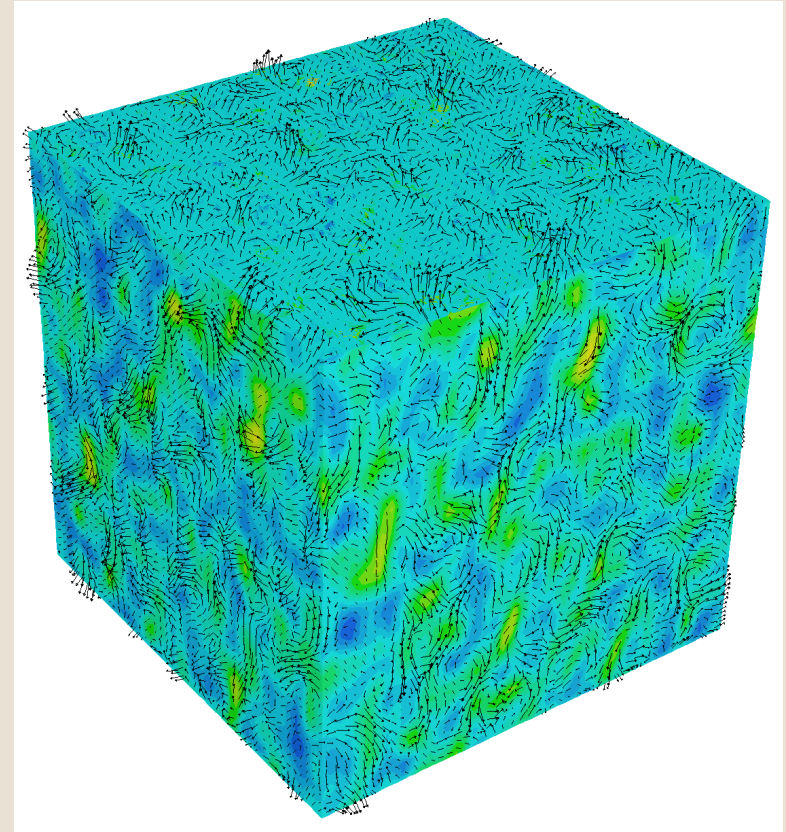


LES predictions of the reattachment point by different methods

	x_r
Exp.	$4.7 H$
Periodic	$5.0 H$
VM	$5.2 H$
Random	$7.7 H$

LES Capability in FLUENT Initial Conditions

- Initial condition for velocity field is generally not important for statistically steady-state flows
- Patching a realistic turbulent velocity field can however help shorten the simulation time substantially to get to a statistically steady state
- The same spectral synthesizer can be used to superimpose turbulence on top of the mean velocity field (new in 6.2).



Velocity field generated by turbulence synthesizer for a homogeneous turbulence

LES Capability in FLUENT

Detached Eddy Simulation (DES)

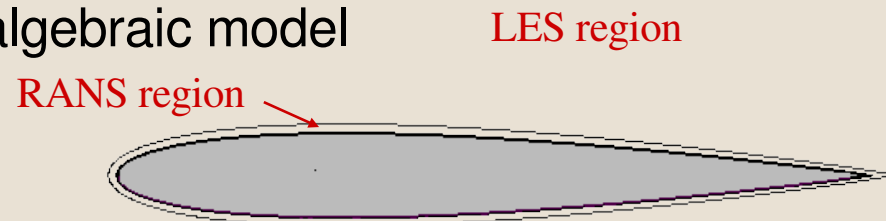
- Motivation
 - Near-wall-resolving LES is prohibitively expensive for high-Re wall bounded flows
 - Using RANS in near-wall regions would significantly mitigate the mesh resolution requirement, reducing the cost
- FLUENT offers a RANS/LES hybrid model based on S-A turbulence model (Spalart *et al.*, 1997)

$$\frac{D\tilde{\nu}}{Dt} = C_{bl}\tilde{S}\tilde{\nu} - C_{wl}f_w\left(\frac{\tilde{\nu}}{\bar{d}}\right)^2 + \frac{1}{\sigma_{\tilde{\nu}}}\left[\frac{\partial}{\partial x_j}\left\{\left(+\rho\tilde{\nu}\right)\frac{\partial\tilde{\nu}}{\partial x_j}\right\} + \dots\right]$$

$$\bar{d} = \min\left(d_w, C_{DES}\right)$$

- One-equation SGS turbulence model
 - In equilibrium, it reduces to an algebraic model

$$\tilde{\nu} \approx \left(C_{DES}\right)^2 S$$



LES Capability in FLUENT

Detached Eddy Simulation (DES)

Model

- Inviscid
- Laminar
- Spalart-Allmaras (1 eqn)
- k-epsilon (2 eqn)
- k-omega (2 eqn)
- Reynolds Stress (7 eqn)
- Detached Eddy Simulation
- Large Eddy Simulation

Spalart-Allmaras Options

- Vorticity-Based Production
- Strain/Vorticity-Based Production

Model Constants

Cdes: 0.65

Cb1: 0.1355

Cb2: 0.622

Cv1: 7.1

Cw2:

User-Defined Functions

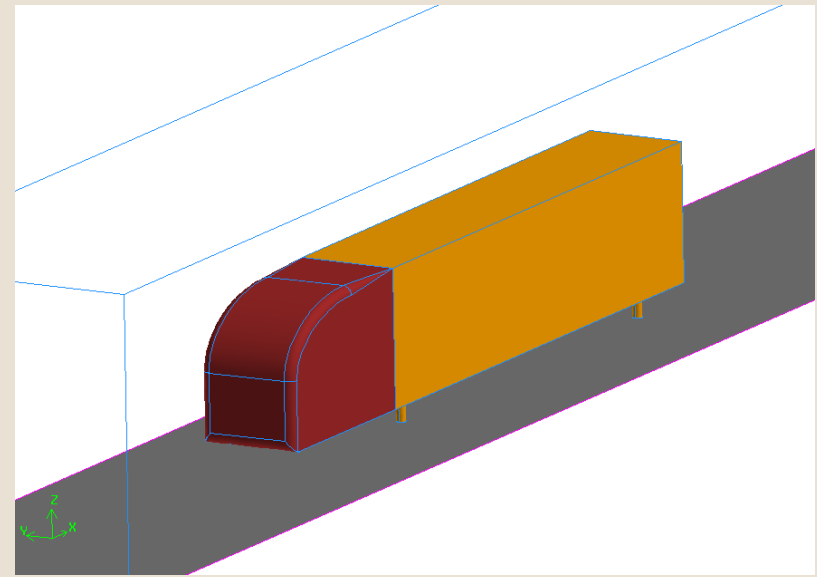
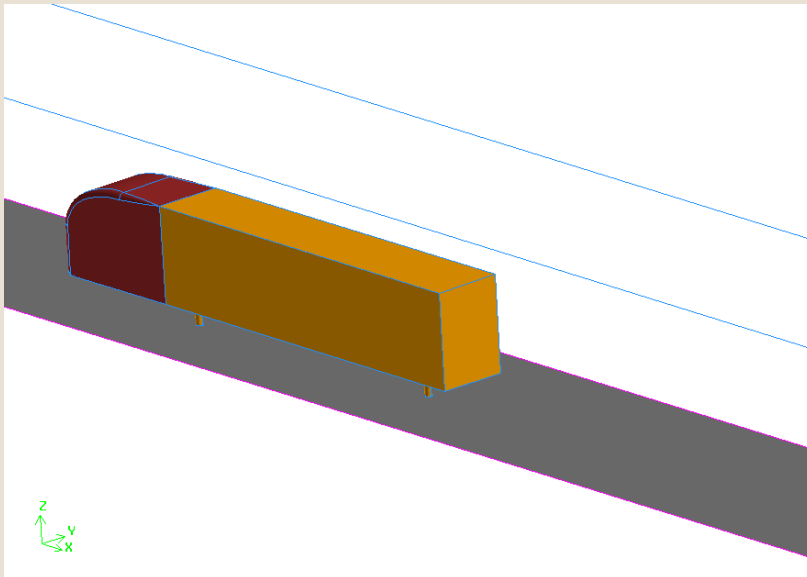
Turbulent Viscosity: none

OK Cancel Help

LES Capability in FLUENT

DES Example: GTS Body (1)

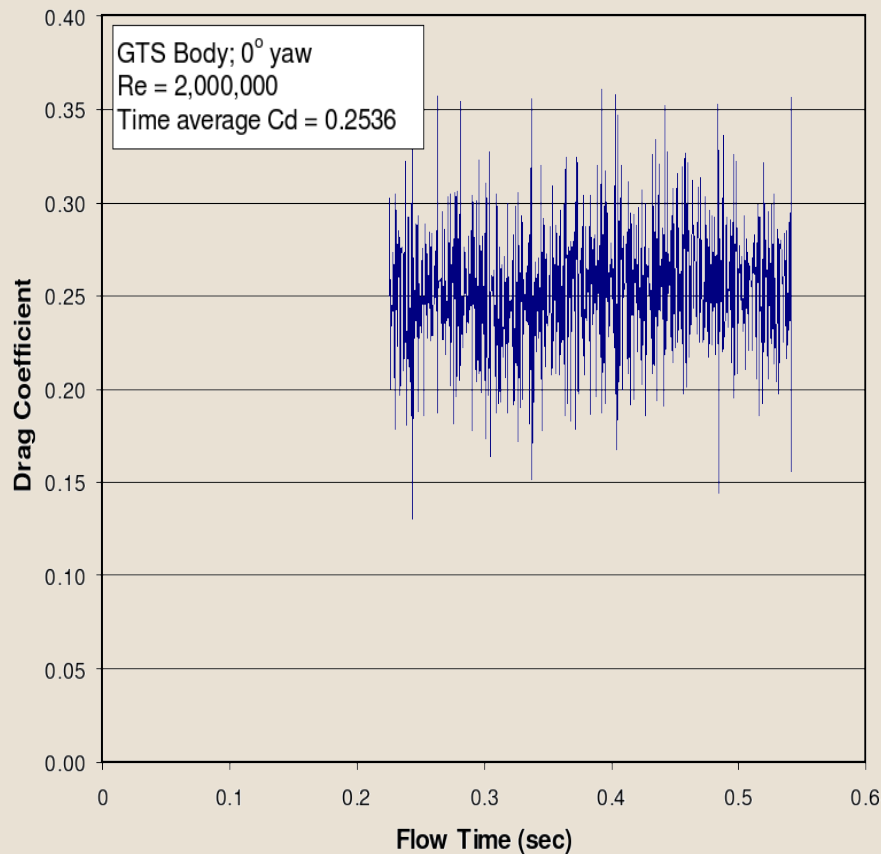
- Simplified truck configuration tested at the NASA Ames wind tunnel.
- $Re_L = 2 \cdot 10^6$
- Computed with 11M-cell hex mesh
- Zero-yaw (head-wind)



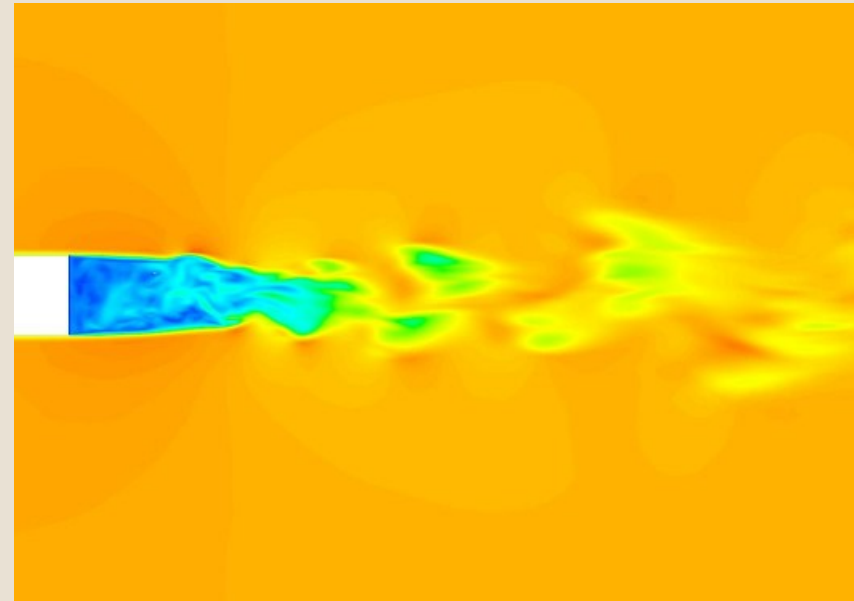
LES Capability in FLUENT

DES Example: GTS Body (2)

- Drag prediction

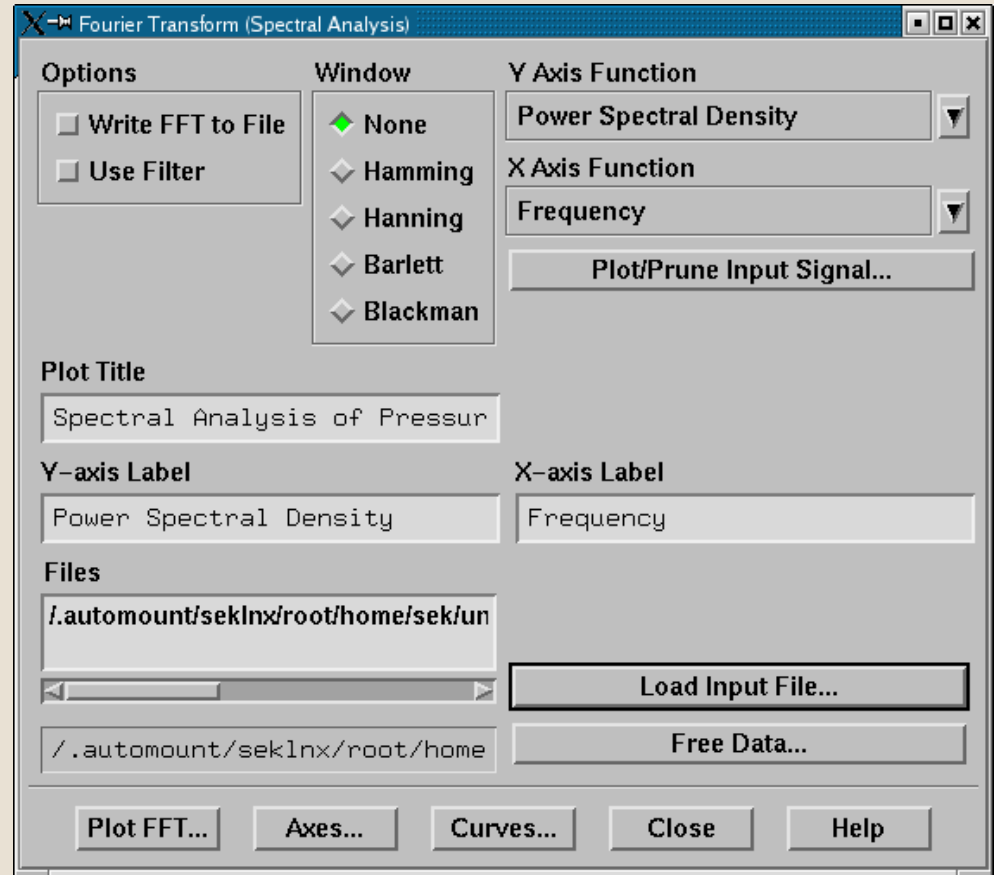


	C_D
Predicted (DES)	0.253
Measured	0.250



LES Capability in FLUENT Postprocessing

- Time-Averaging
 - Mean values of the solution variables.
 - RMS values of the solution variables
- Built-in FFT
 - Data conditioning
 - Pruning
 - Windowing
 - Power spectral density of arbitrary variables



Best Practice LES in FLUENT

General Tips



- Mesh
 - Use hex meshes for the best accuracy
 - Take advantage of hybrid meshing capability and local mesh refinement
- Spatial discretization
 - Stick with CD or BCD for momentum
 - Use the node-based gradient option
 - Use the upwind schemes (QUICK, MUSCL, SOU) for scalars
- Time discretization
 - Use the second-order scheme
 - Use the NITA/fractional-step method for incompressible or weakly compressible flows
 - With the fully-iterative scheme, use SIMPLEX (jack up URF's – 0.9 for pressure and momentum equations)
- SGS modelling
 - The dynamic Smagorinsky's model is a good starting point.
 - Consider DES for high-Re wall-bounded flows

Best-Practice LES with FLUENT Recommended Procedure (1)



- Compute the mean flow with steady RANS
- Superimpose the synthesized turbulence on the mean flow
TUI: `/solve/initialize/init-instantaneous-vel`
- Switch to LES, select the SGS turbulence model of your choice
- Select the solver algorithm (e.g., ITA/NITA, FSM/PISO/SIMPLEC) and the discretization schemes
- Set the time-step (Δt) and adjust the solver parameters if needed (e.g., URF's, convergence criteria)
- Set the monitors with relevant global (e.g., forces/moments) and local quantities (e.g., velocity, pressure) of your choice
- Set the autosave of the data files (e.g., every a few hundreds time-steps)

Best-Practice LES with FLUENT

Recommended Procedure (2)



- Save the viewgraphs of your choice for animation (contours of pressure, iso-surfaces of vorticity, second-invariant, etc.)
- Start the transient run and continue until a statistically steady state is reached
- Start sampling the data (to compute mean and r.m.s. values)
GUI: Solve/Iterate... (click on the “Data Sampling for Time Statistics” button)
GUI: Solve/Initialize/Reset Statistics to reset the data sampling
- Continue sampling for a sufficiently long period of time
- Post-process the results (mean, r.m.s., power spectra, etc.)

Closing Remarks



- RANS-based turbulence models are still the workhorse for industrial CFD, and will be so for some time
- In the coming years, high-fidelity CFD will rely upon less “modelling” and more “simulation”
- LES is rapidly becoming feasible for industrial flows
- FLUENT has been significantly upgraded recently in numerics and subgrid-scale turbulence modelling
- Our goal is to ramp up the overall efficacy of LES to the level where LES becomes a useful tool for industrial applications.